

Ruminations on a convective theme

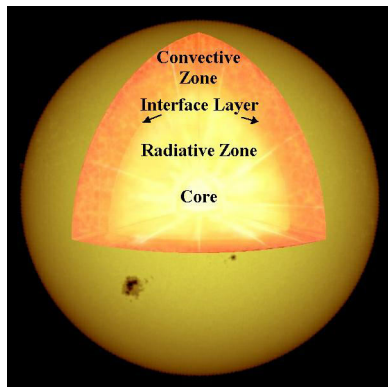
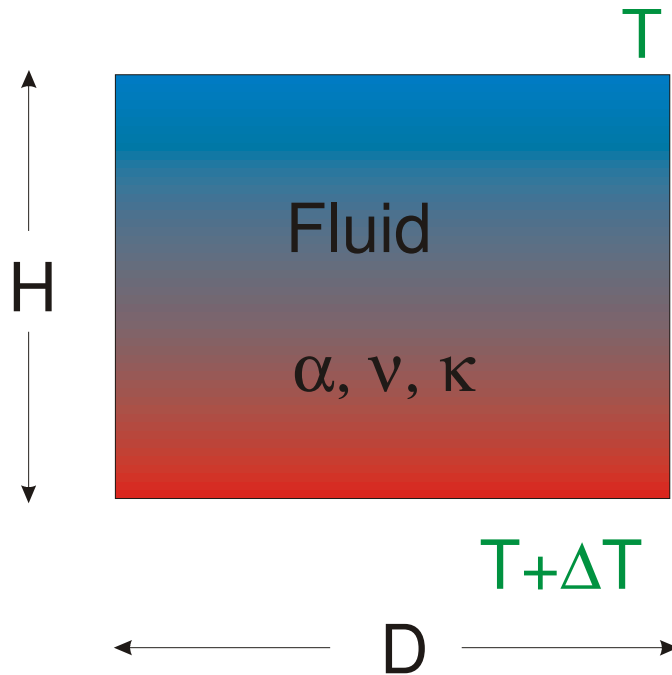
J. Niemela

ICTP Trieste

Sreeni helping celebrate Russ Donnelly's 65th birthday in 1995 in Boulder CO. Carl Weiman was also there to talk about his BEC observations a few weeks earlier



Rayleigh-Benard Convection

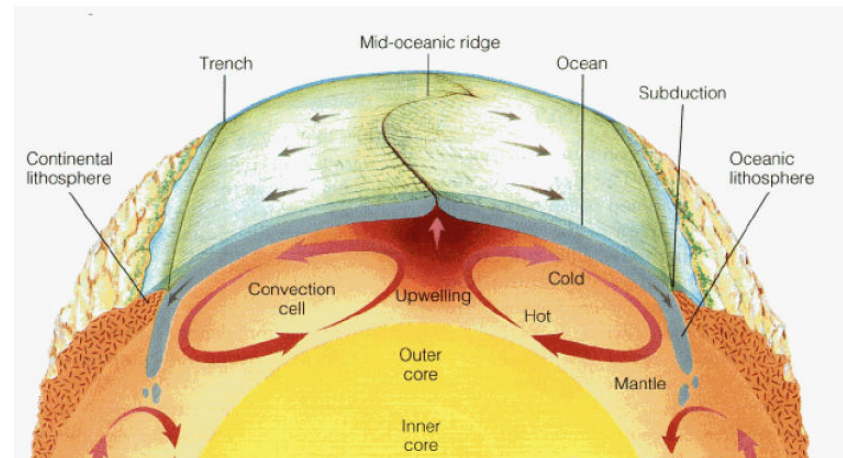


Notation used in this talk

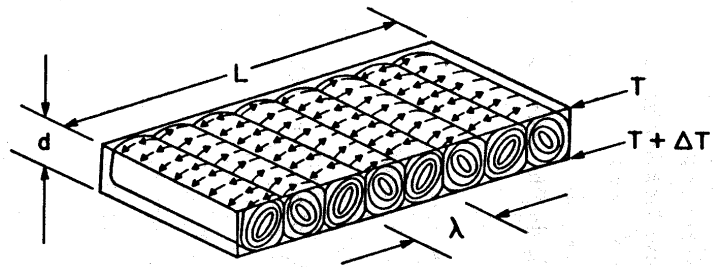
$$\text{Ra} = \frac{g \alpha \Delta T H^3}{\nu \kappa} \quad \text{Rayleigh number}$$

$$\text{Pr} = \frac{\nu}{\kappa} \quad \text{Prandtl number}$$

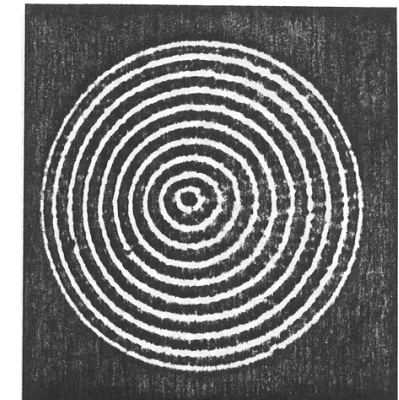
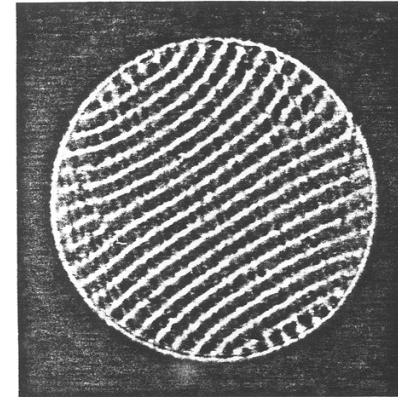
$$\Gamma = \frac{D}{H} \quad \text{Aspect ratio}$$



Rayleigh Benard convection (RBC) *near onset*: For the most part, a completely understood problem



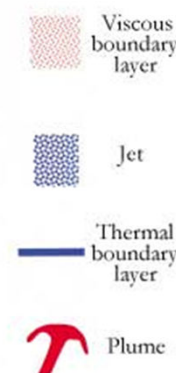
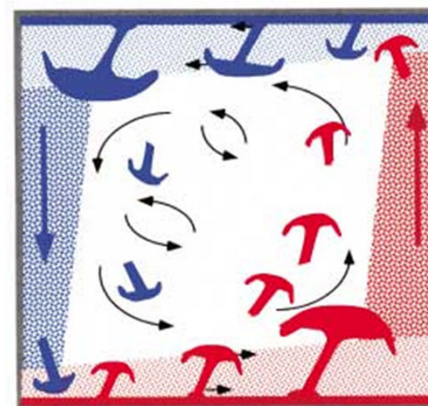
Boundary conditions make a difference



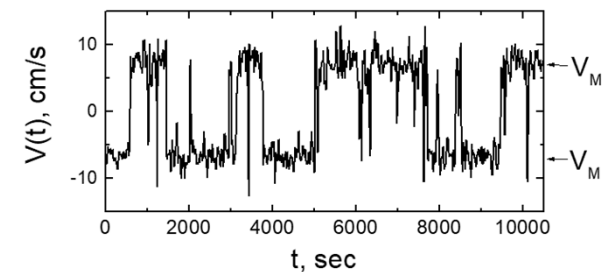
RBC at very high Ra: **Plumes** figure prominently



FIGURE 1. Photographs of thermals rising from a heated horizontal surface.

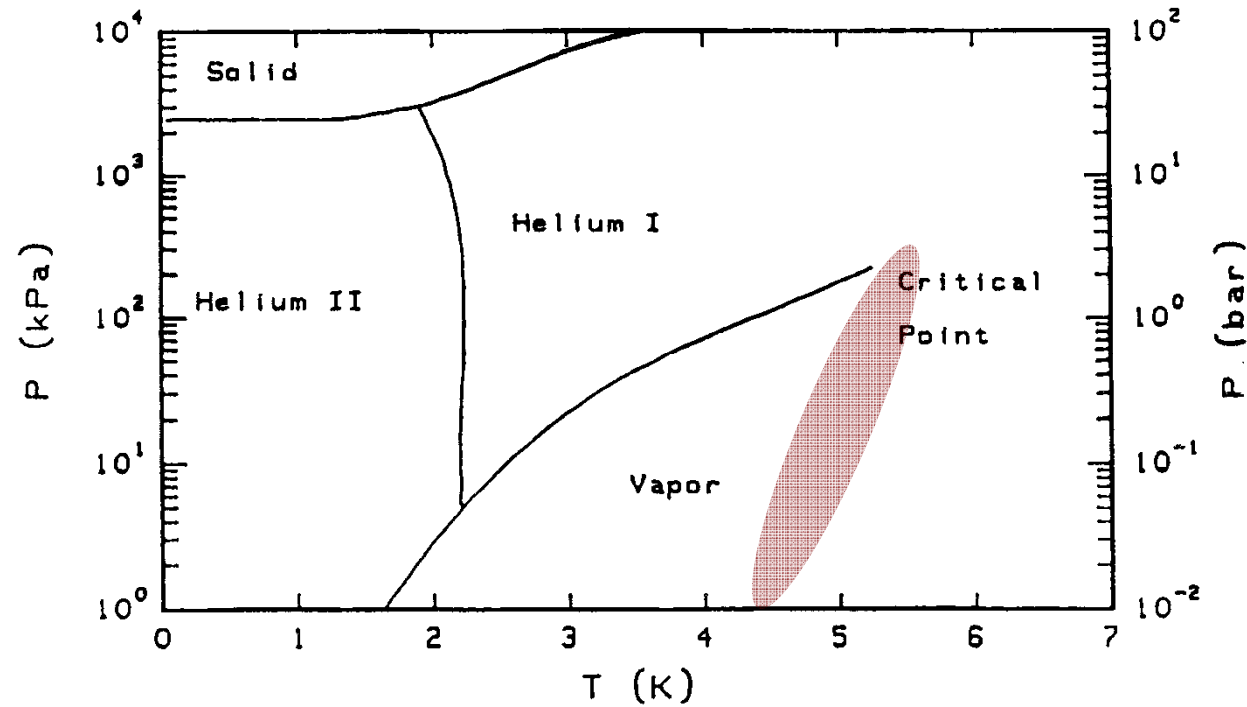


Mean wind "reversals"



(from L. Kadanoff, Physics Today, August 2001)

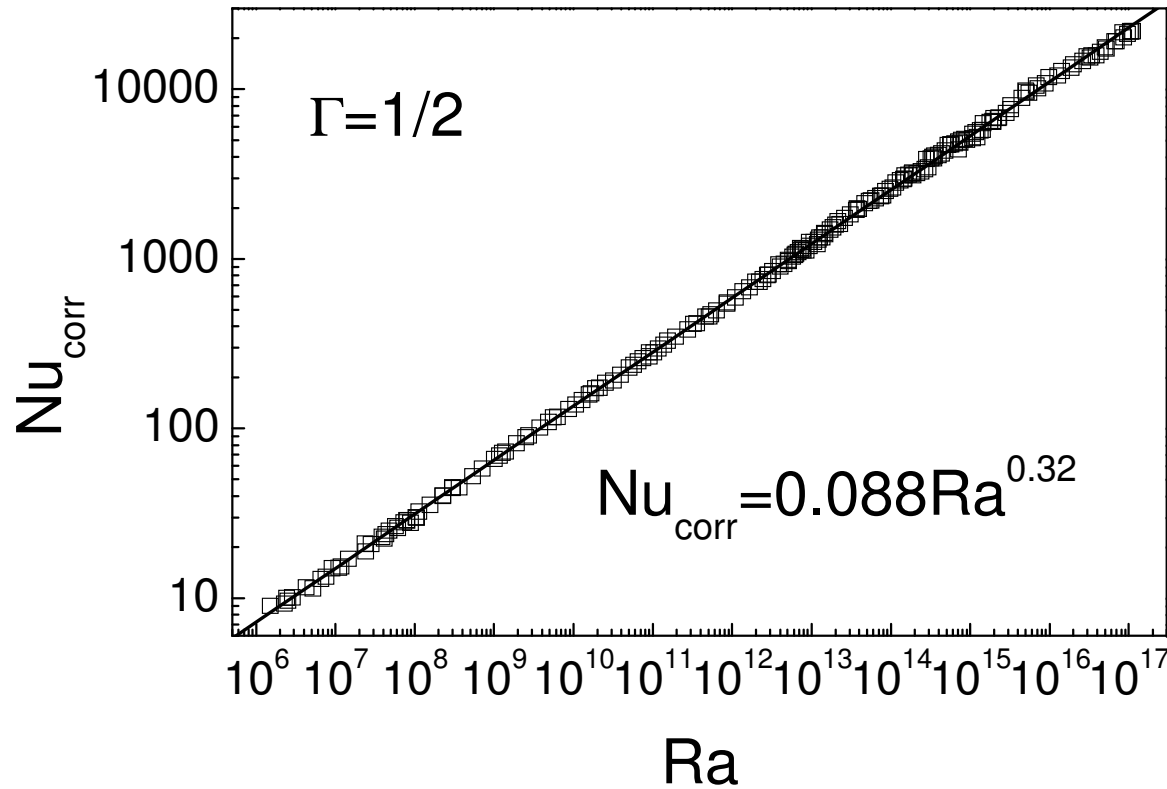
Using helium to obtain high Ra



12 orders of magnitude variation in Ra in shaded region. Desire all 12
in the turbulent regime (scaling and high Ra)

Turbulent Heat Transfer I

Conductivity enhancement by a factor of 20,000



“From a distance all
cows look black”

(1) JJN, L. Skrbek, K.R. Sreenivasan & R.J. Donnelly, *Nature*, **404**, 837 (2000)

(2) JJN & K.R. Sreenivasan, *J. Fluid Mech.*, **557** 411-422 (2006).

Turbulent heat transfer II (with slight hand motions)

advection-diffusion equation

$$\frac{\partial T}{\partial t} + U_j \frac{\partial T}{\partial x_j} = \kappa \frac{\partial^2 T}{\partial x_j \partial x_j}$$

Decomposition and averaging over fluctuations yields for the vertical heat flux

$$q_3 = \rho c_p \left(\overline{\theta u_3} - \kappa \frac{\partial \bar{T}}{\partial x_3} \right)$$

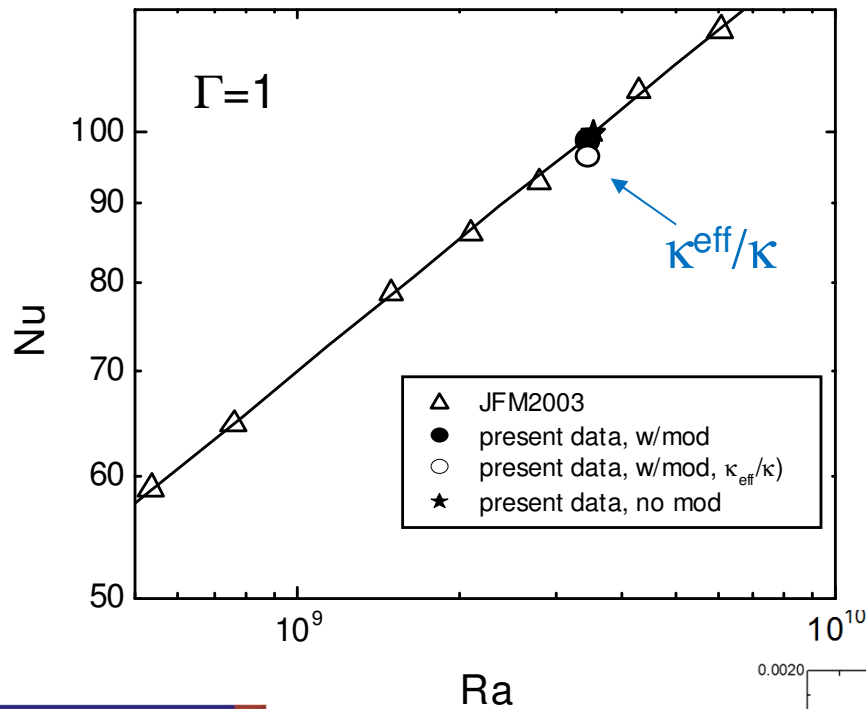
$$\overline{\theta u_3} \equiv -\kappa_T \frac{\partial \bar{T}}{\partial x_3}$$

a *convenient definition* treating turbulence as a diffusive “fluid” (thanks Charles, for opening up the “can of sand”)

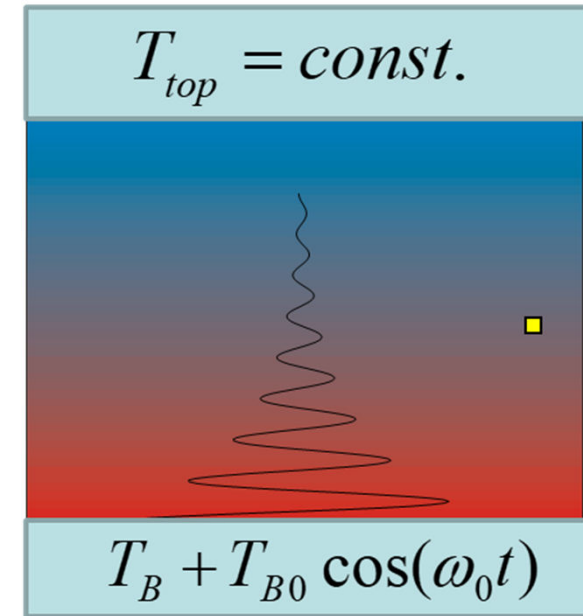
$$\boxed{Nu = \frac{\kappa^{eff}}{\kappa}}$$

$$\kappa^{eff} \equiv (\kappa + \kappa_T)$$

Works pretty well....(open circle)



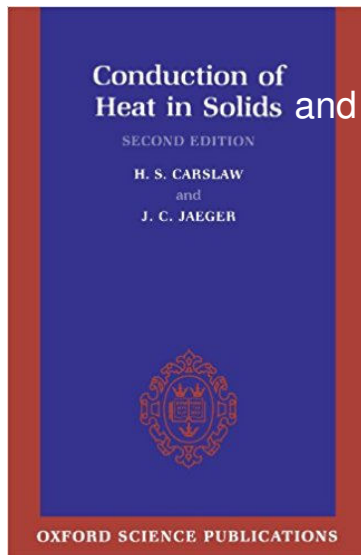
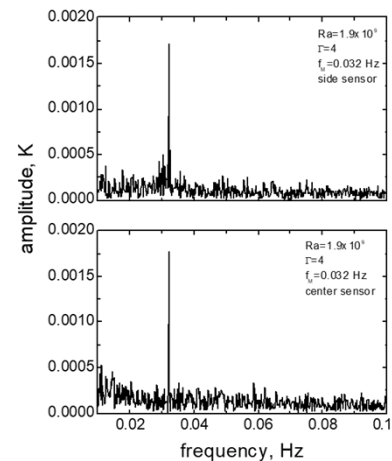
How was κ^{eff} measured?



$$\frac{\partial T}{\partial t} = \kappa^{eff} \frac{\partial^2 T}{\partial x_j \partial x_j}$$

$$T(z, \omega_0) = (T_{B0}) \exp(-z / \delta_s)$$

$$\delta_s = \sqrt{\frac{2\kappa^{eff}}{\omega_0}}$$



JJN, K.R. Sreenivasan, Phys Rev. Lett., **100**, 184502 (2008)

Rotation about vertical axis:

Rotation plays a large role in large scale geophysical turbulent flows

Rotation rate: Ω_D (rad/s) \longrightarrow Dimensionless rotation rate: $\Omega \equiv \left(\frac{2\Omega_D H^2}{\nu} \right) = Ek^{-1}$

Taylor number: $Ta = \Omega^2 = Ek^{-2}$

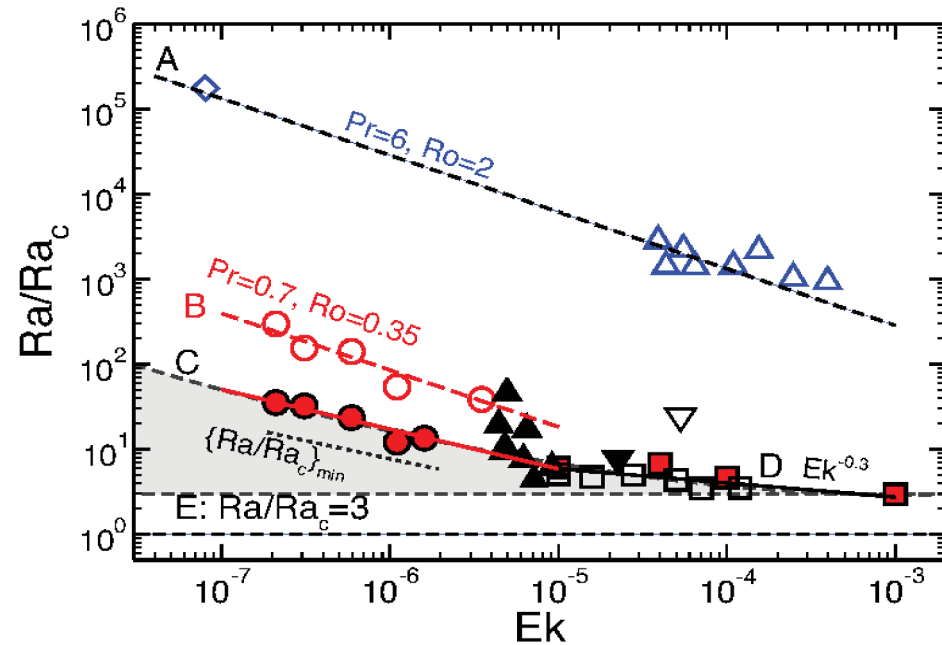
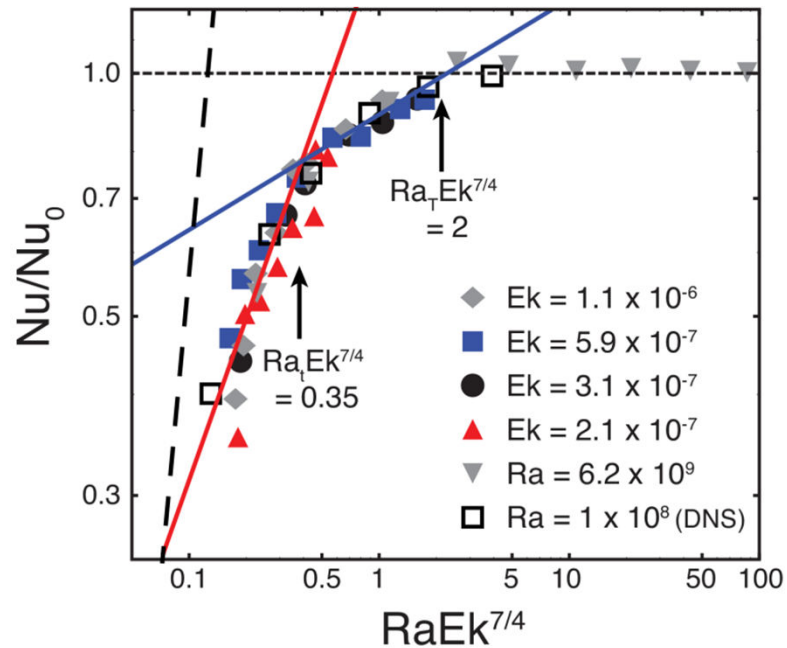
Convective Rossby number: $Ro = \left[\frac{Ra}{PrTa} \right]^{1/2} = (2\Omega_D)^{-1} \left(\frac{g\alpha\Delta T}{H} \right)^{1/2}$



Turbulent heat transfer III

Heat transport in the geostrophic (rotation-dominated) regime

At constant Ek, or Ra



$Nu \sim Ra^1$ in geostrophic regime (but limited range for scaling)

JJN, S. Babuin, K.R. Sreenivasan, J. Fluid Mech. **649**, 509-522 (2010)

R.E. Ecke, JJN, Phys. Rev. Lett. **113**, 114301 (2014)

Here are some of the things Najmeh Foroozani might have talked about:



Effect of wall roughness on the large scale circulation in turbulent convection with cubic confinement

N. Foroozani¹, JJN, V. Armenio², K. R. Sreenivasan³

¹International Centre for Theoretical Physics (ICTP), ²University of Trieste,

³New York University USA (NYU)

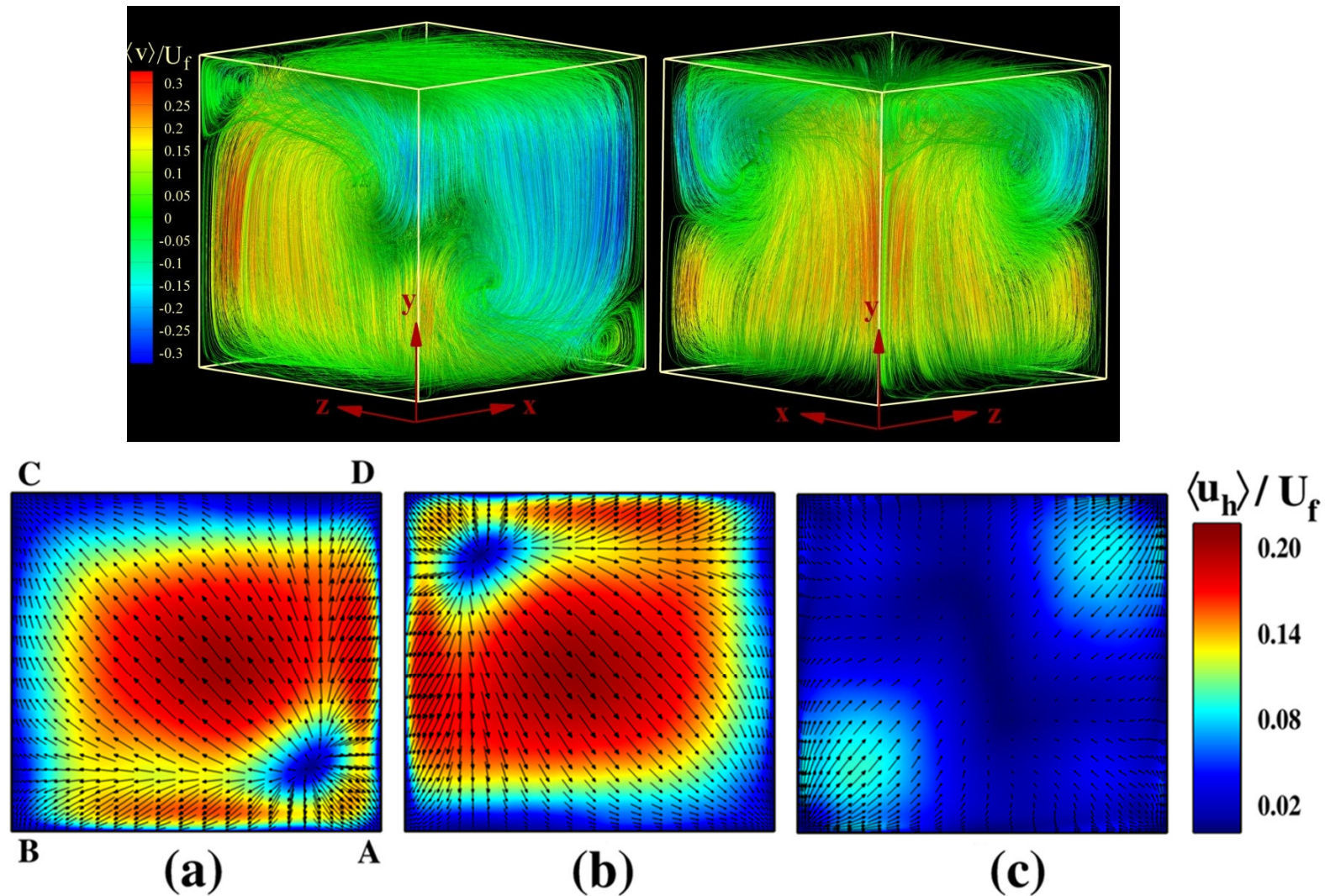
Mathematical Model

Large Eddy Simulations (LES) are used, solving the spatially filtered Boussinesq approximation of the unsteady NS equations in 3D (Armenio, Meneveau,...)

Boundary conditions and computational domain

- Cubic cell ($\Gamma=1$), **No slip** condition, **adiabatic** side walls, **isothermal** top and bottom walls with $Pr = 0.7, Ra = 10^6 \text{ \& } 10^8$.
- Density is a linear function of temperature: $\rho = \rho_0[1 - \alpha(T - T_0)]$
- For *low* Ra , grid mesh $32 \times 64 \times 32$ & for *high* Ra $64 \times 96 \times 64$.
- Grid cells clustered near walls to resolve properly momentum and thermal boundary layers.
- Normalization scales for lengths, velocity, density, time respectively: H , $U_f = \sqrt{\alpha g \Delta T H}$, $\Delta \rho = \rho_{top} - \rho_{bot}$ and $T_{eddy} = 2H/v_{rms}$

Features of the Large Scale Flow in a Cube ($Ra=10^8$)

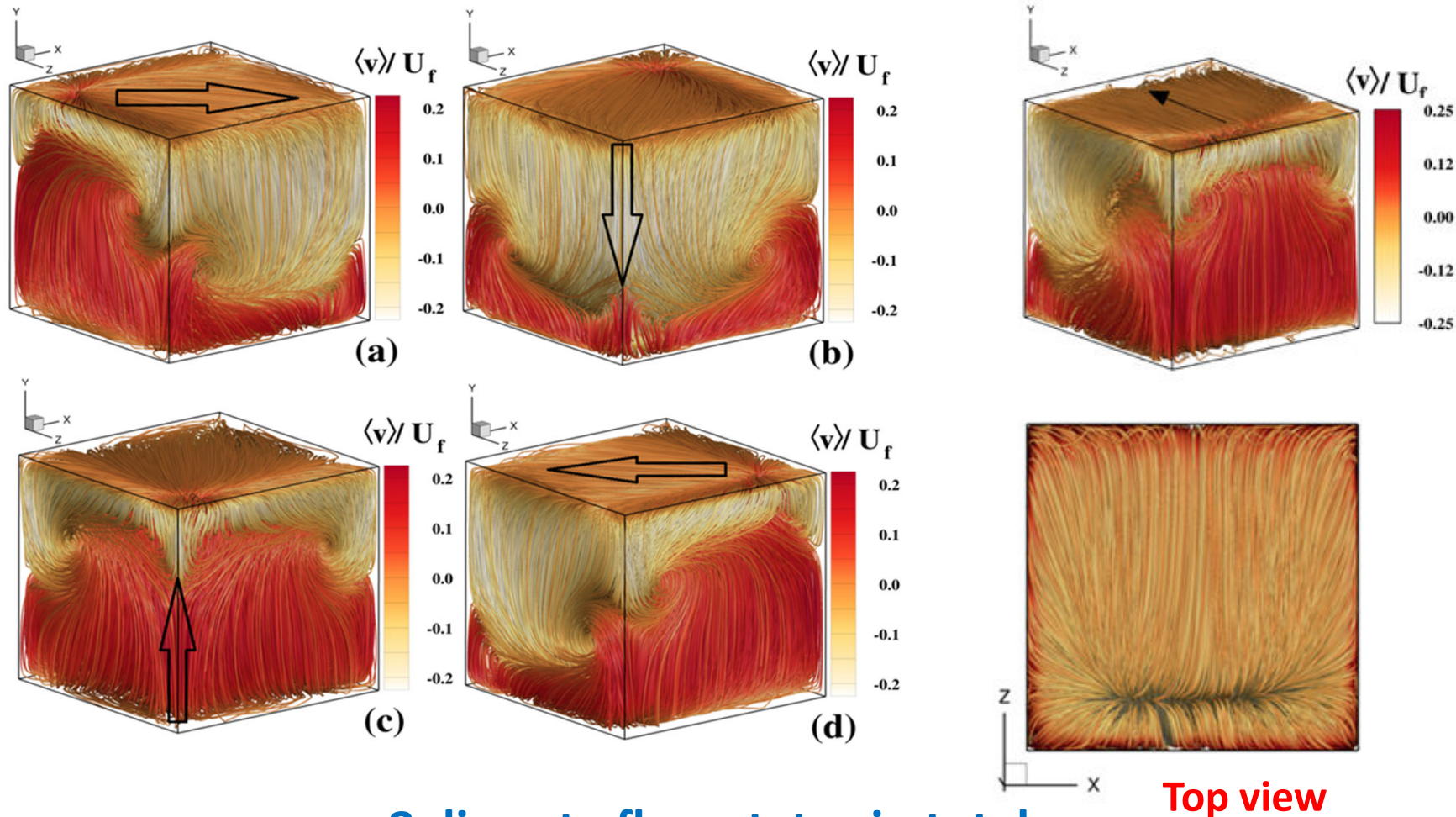


N. Foroozani, JJN, V. Armenio, and K. R. Sreenivasan, Phys. Rev. E **90**, 063003 (2014)

N Foroozani, JJN, V Armenio, KR Sreenivasan, Physical Review E **95** (3), 033107 (2017)

Re-orientations of the Large Scale Flow in a Cube, $Ra=10^8$

Transient states in between,
parallel to side wall

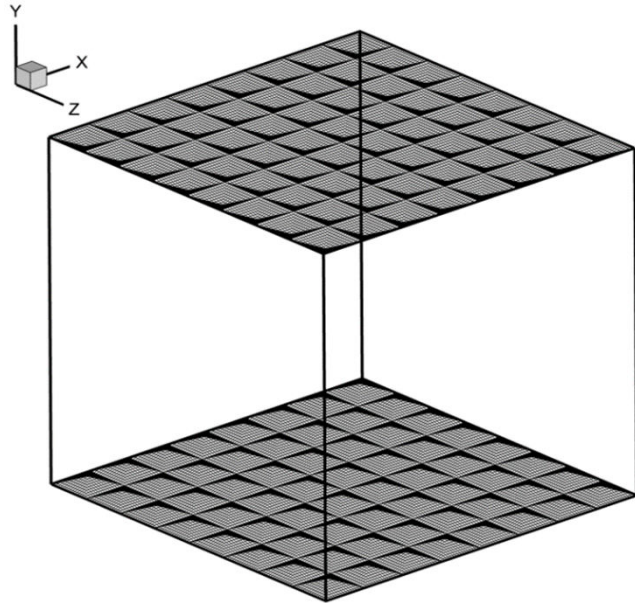


8 discrete flow states in total

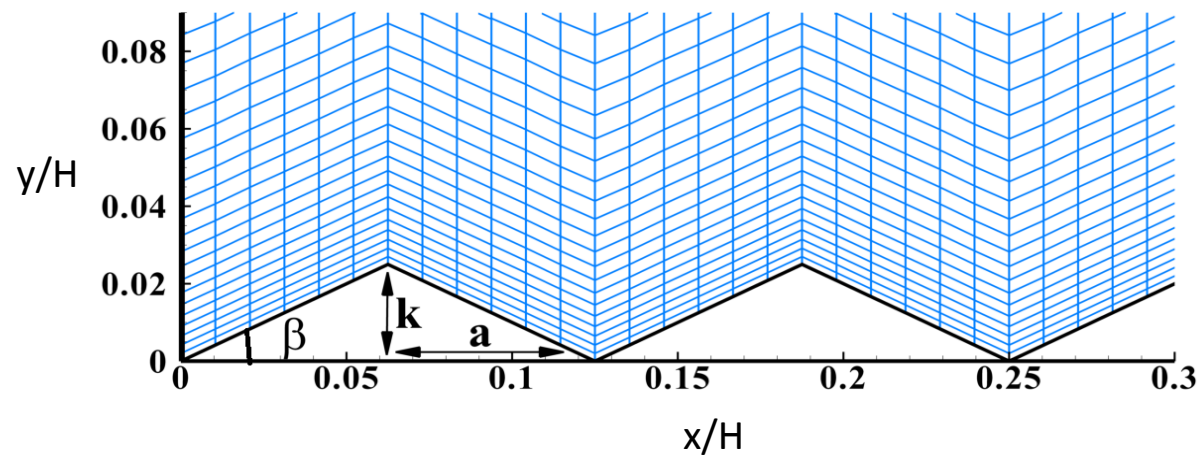
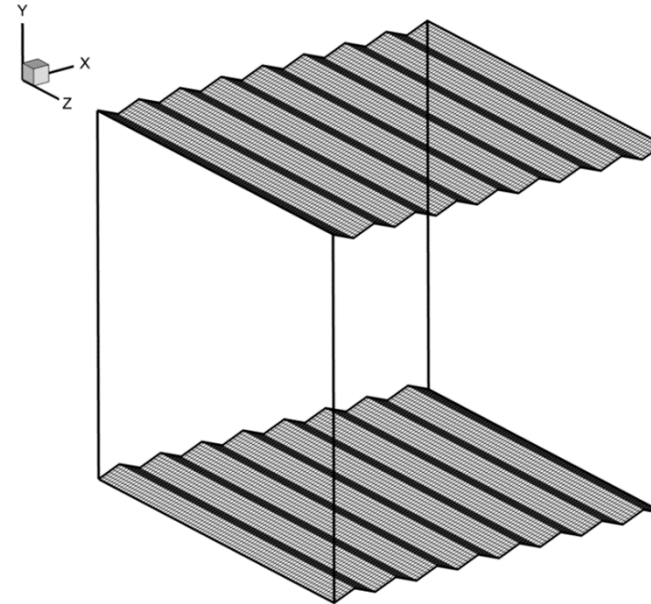
N. Foroozani, J. J. Niemela, V. Armenio, and K. R. Sreenivasan Phys. Rev. E 95, 033107 (2017)

Adding “2D” and 3D roughness elements

Pyramids (64)

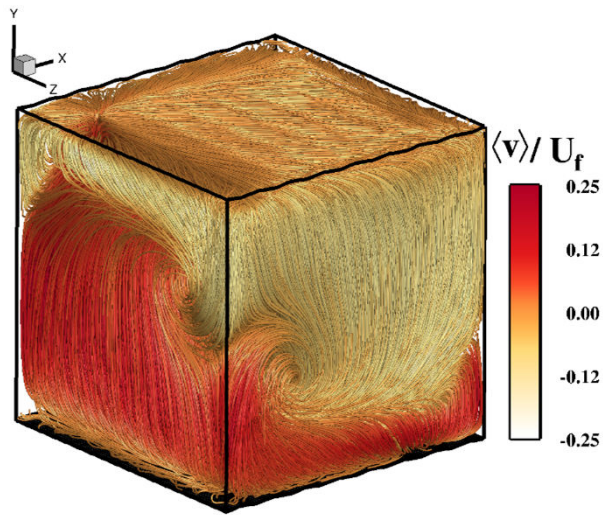


Grooves (8)

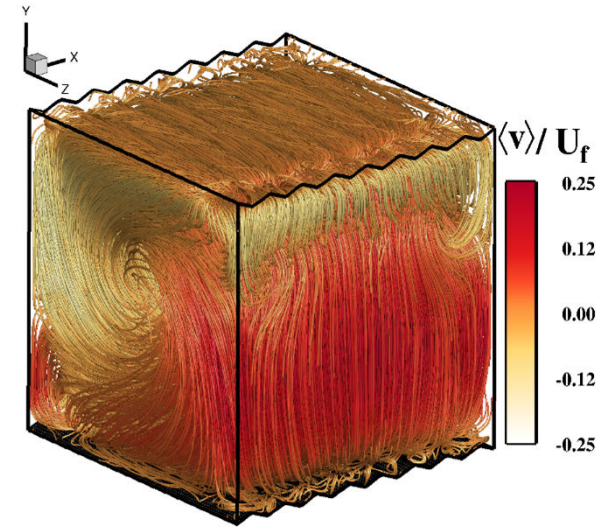


Grid mesh:
 $96 \times 96 \times 96$

Grooves

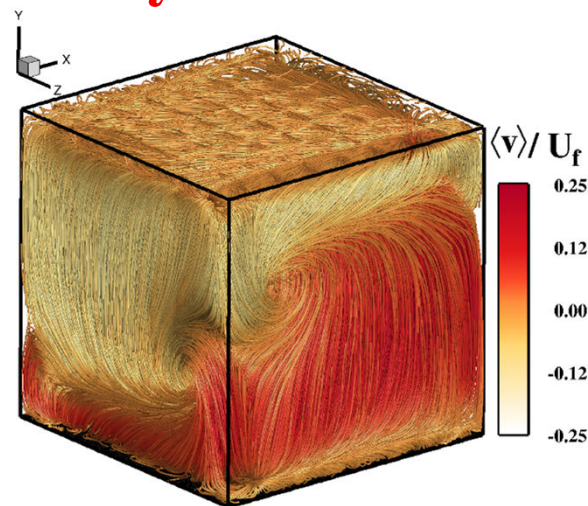


Hydrodynamically **smooth**



Hydrodynamically **rough**

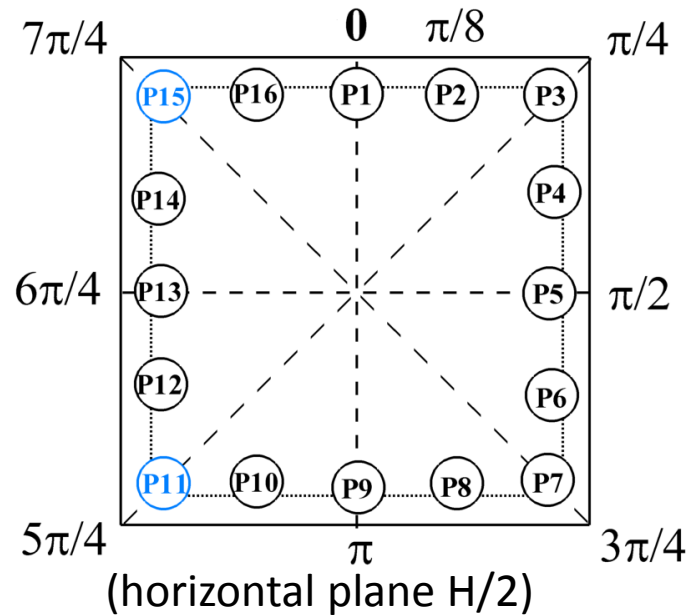
Pyramids



Hydrodynamically **rough** (same configuration as for smooth)

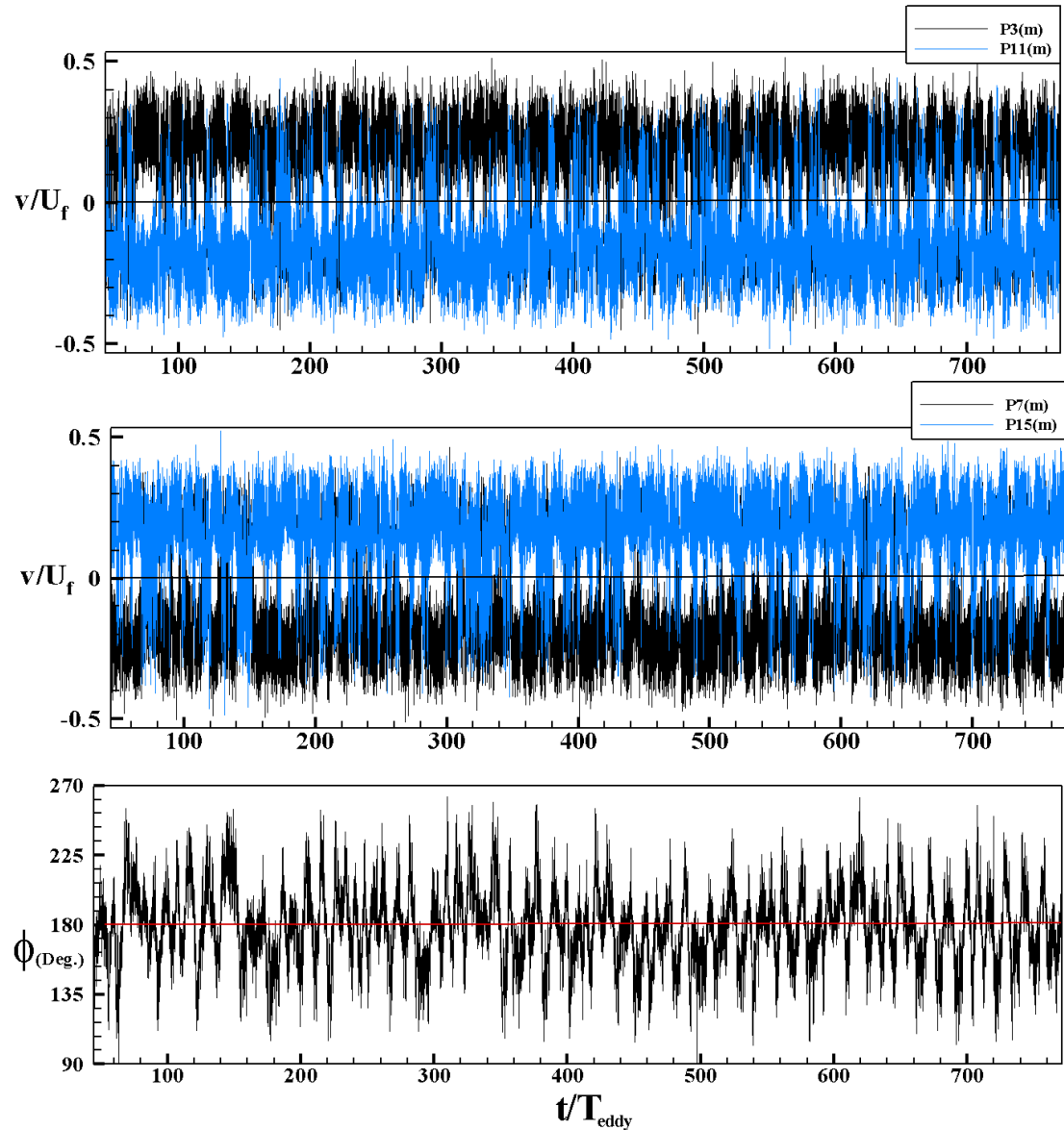
Unsteady flow states with (hydrodynamically rough) *grooves*

Velocity probe placement

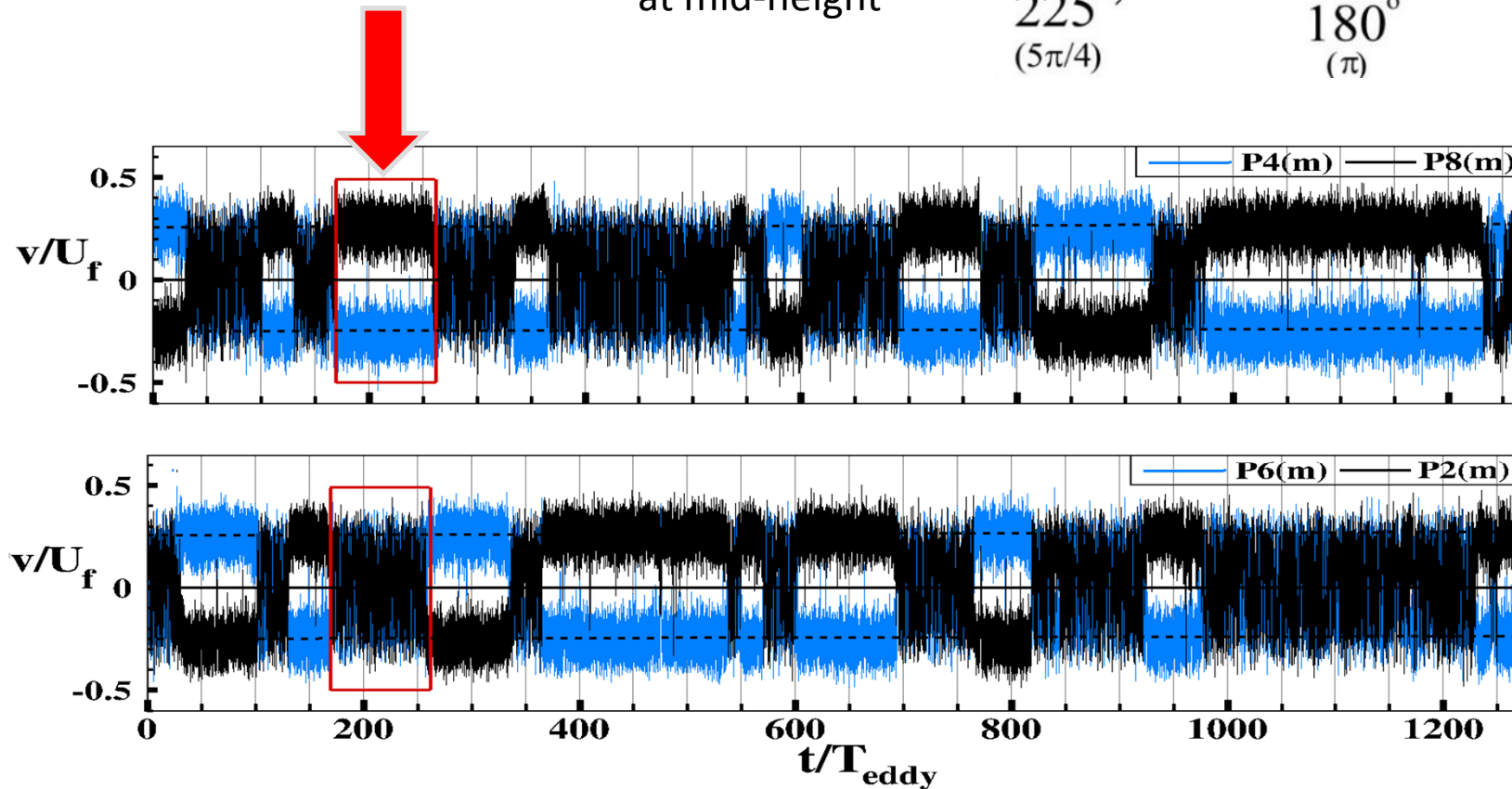
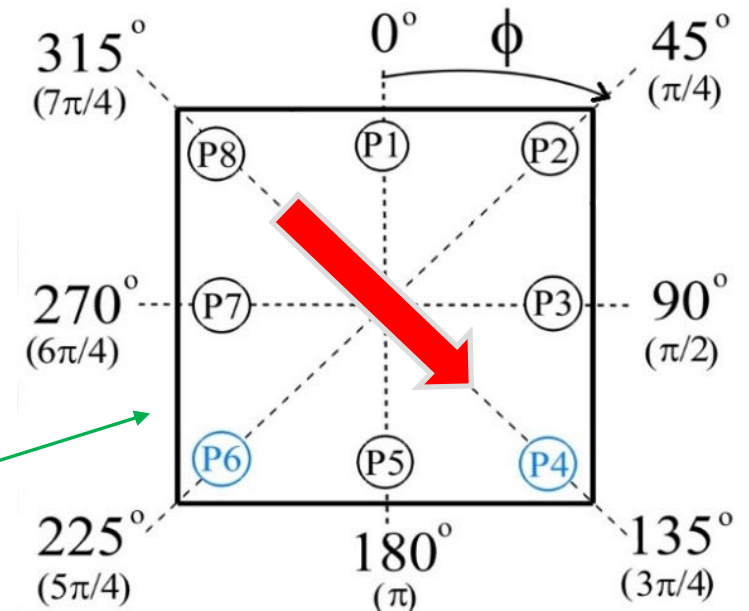


Time averaged flow is
parallel to side wall

Fourier Transform

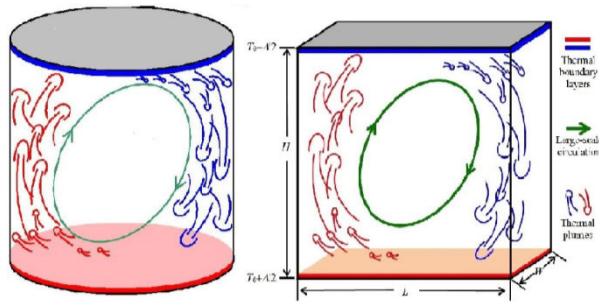


Flow with smooth boundaries:
Non-periodic re-orientations observed
but no direct reversals



ASIDE: Q. Does container shape affect rms statistics in the bulk?

A. Yes (Daya and Ecke [*Phys. Rev. Lett.* **87**, 184501 (2001)])



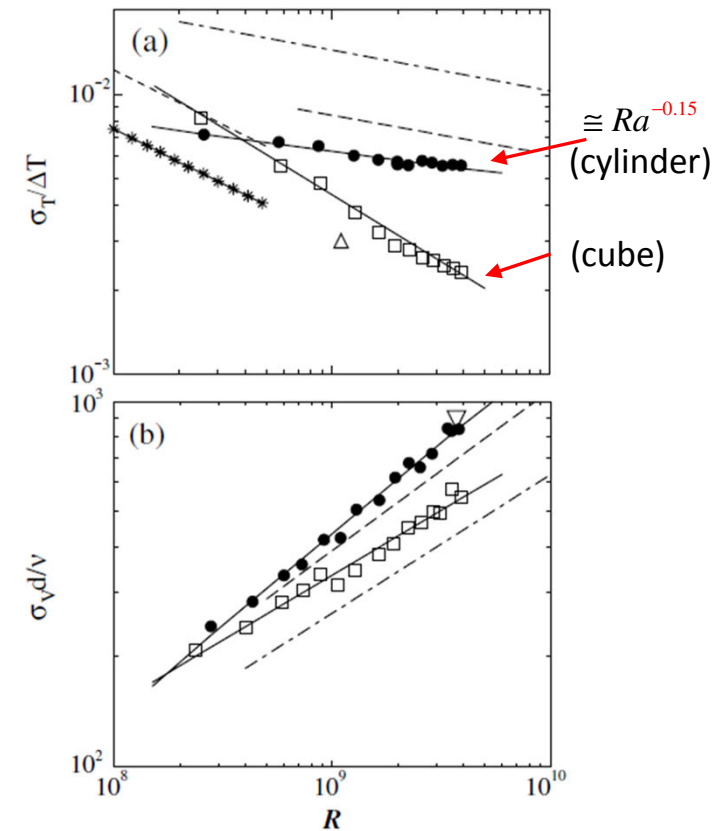
Daya and Ecke found in **cube**:

$$\frac{\sigma_T}{\Delta T} \propto Ra^{-0.48 \pm 0.03} \quad \frac{\sigma_V H}{\nu} \propto Ra^{-0.36 \pm 0.05}$$

Our results in a cube:

$$\frac{\sigma_\rho}{\Delta \rho} = 0.59 Ra^{-0.46} \quad \frac{\sigma_V H}{\nu} = 0.32 Ra^{0.39}$$

N. Foroozani, JJN, V. Armenio, and K. R. Sreenivasan,
Phys. Rev. E **90**, 063003 (2014).



From Daya and Ecke 2001

Conclusions



“Simple fluids are easier to drink than understand.”

--**A.C. Newell** and **V. E. Zakharov**, in Turbulence: A Tentative Dictionary (Plenum Press, NY 1994)



“Simple fluids are easier to understand if you drink.”

J. Dudley and JJN, (somewhere in London 2016)



THANKS!

