



Revisiting capillary rise experiments

Can evaporation limit it?

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Overview

1. Introduction
2. Previous works – Relation to **cooling** systems
3. Experimental setup
4. Results
5. Conclusions

Problem statements

Competition b/w evaporation and surface tension
Capillary rise / spreading in **varying** c/s area porous systems

Questions to be answered

Q1. Horizontal Capillary – *Will it spread till infinity?*

Q2. Capillary length V/H porous medium – *What limits it?*

Static parameters – Gravity / Viscosity / Capillary length

Dynamic parameter – **Evaporation**

Q3. Exposed porous medium – *Is evaporation a limiting parameter?*

Notable Works

Lucas (1918) & Washburn (1921) - Lucas-Washburn law - the distance penetrated by a liquid in an initially gas-filled lyophilic capillary tube placed horizontally.

$$h \propto t^{1/2}$$

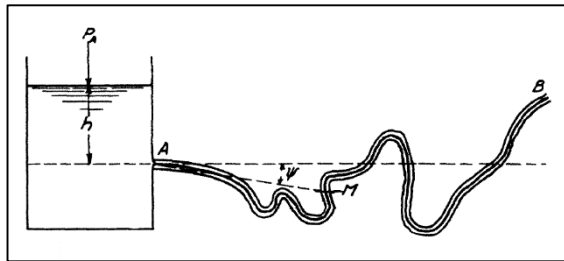
Levine (1980) – Quite complicated relation between the liquid penetration depth and time .

Ponomarenko (2011) - capillary rise in a corner.

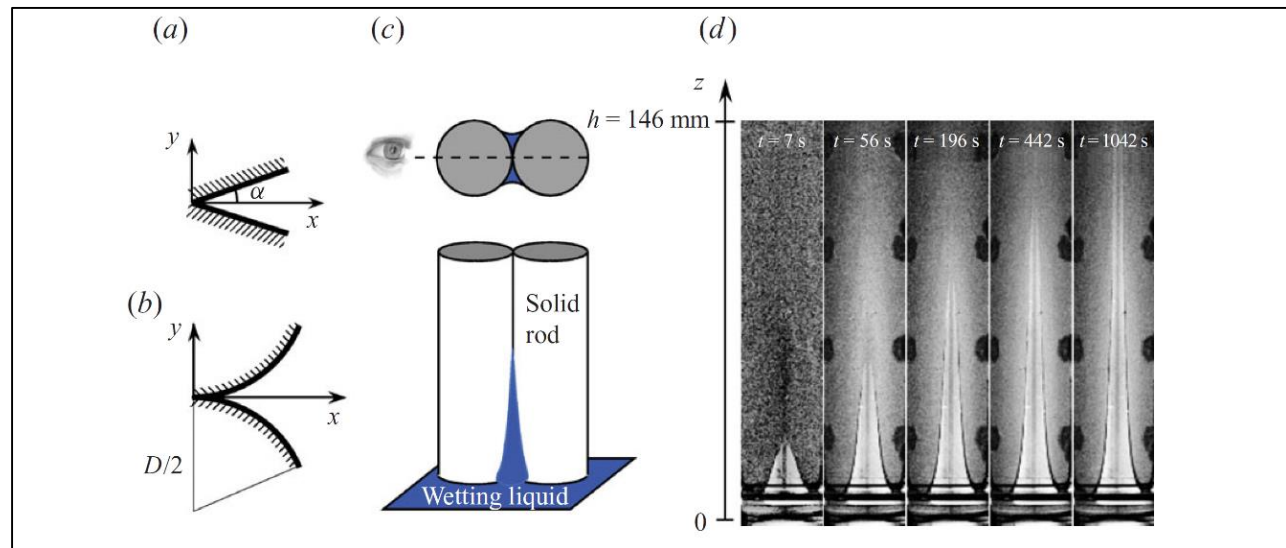
$$h \propto t^{1/3}$$

Vertical Corner

Horizontal Capillary



Washburn (1923)

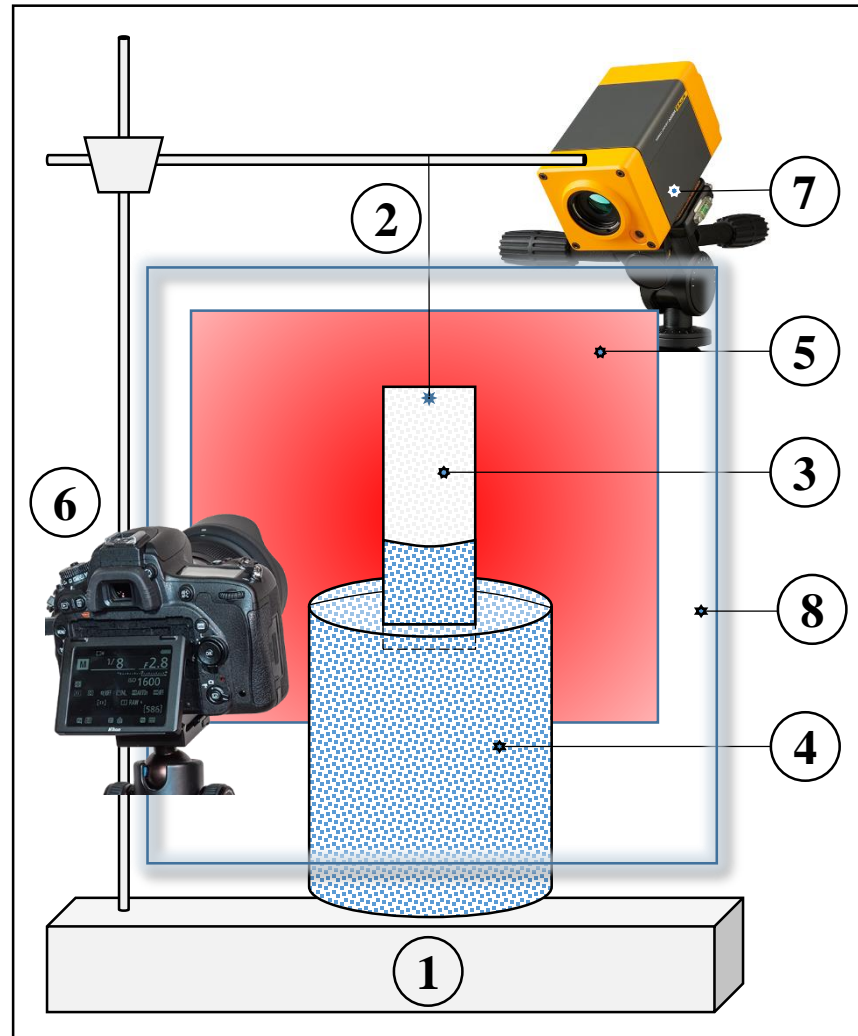


Ponomarenko (2011)

A filter paper – **Complicated** – Combination of capillaries and **corners** (joints of strands)

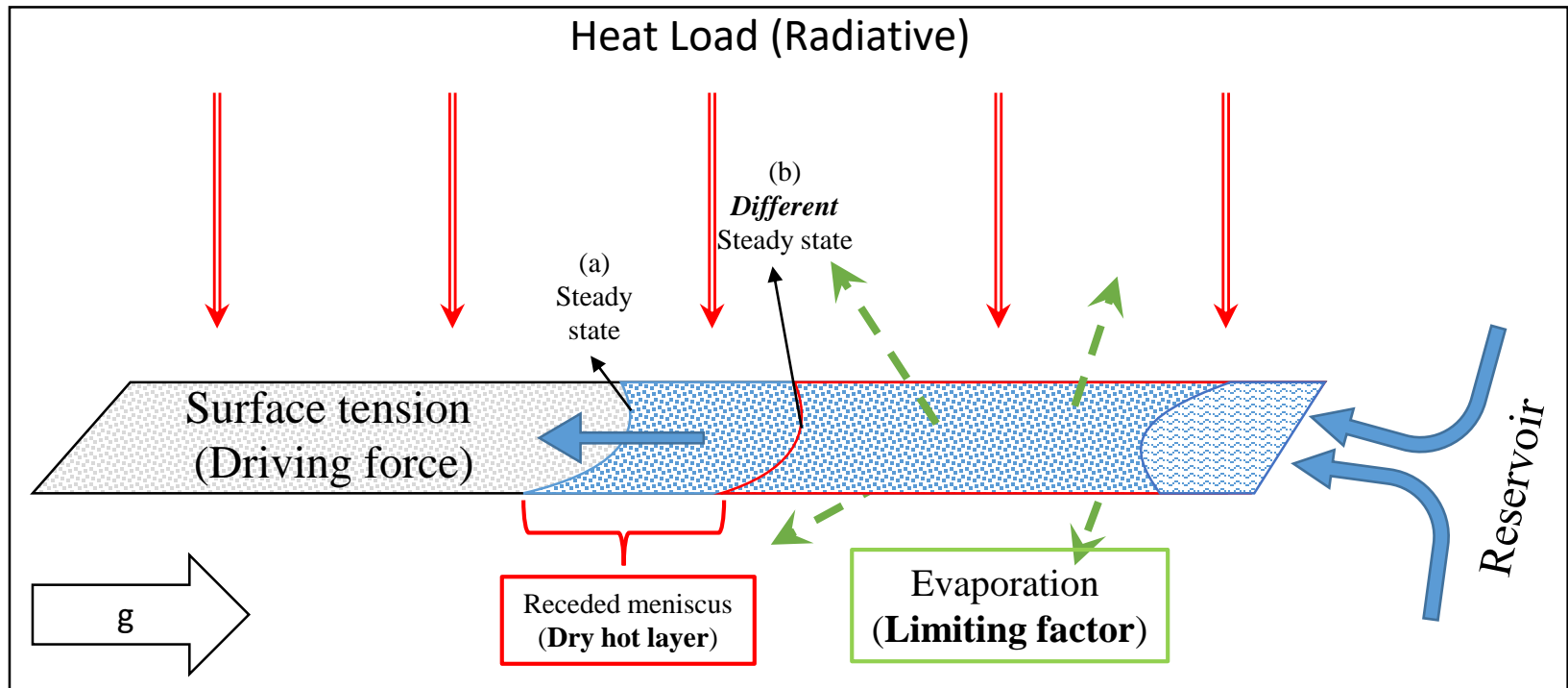
Experimental Setup & Method

1. Stand
2. Pin
3. Filter paper
4. Beaker
5. Heater
6. Optical Camera
7. Thermal Camera
8. Glass



Digital Image Processing
IR images & Videos
Full-scale data analysis

Mechanism



Drawbacks in case (b):

(a) Near-top high temperature

(c) Lower evaporation rate (cooling)

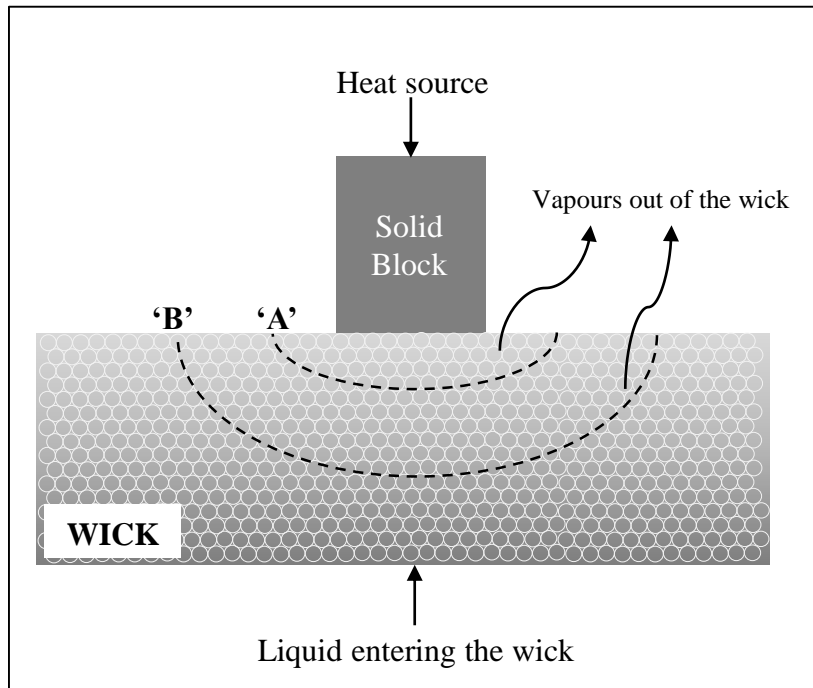
(b) Lower heat transfer to the interface

(d) Increased operating temperature

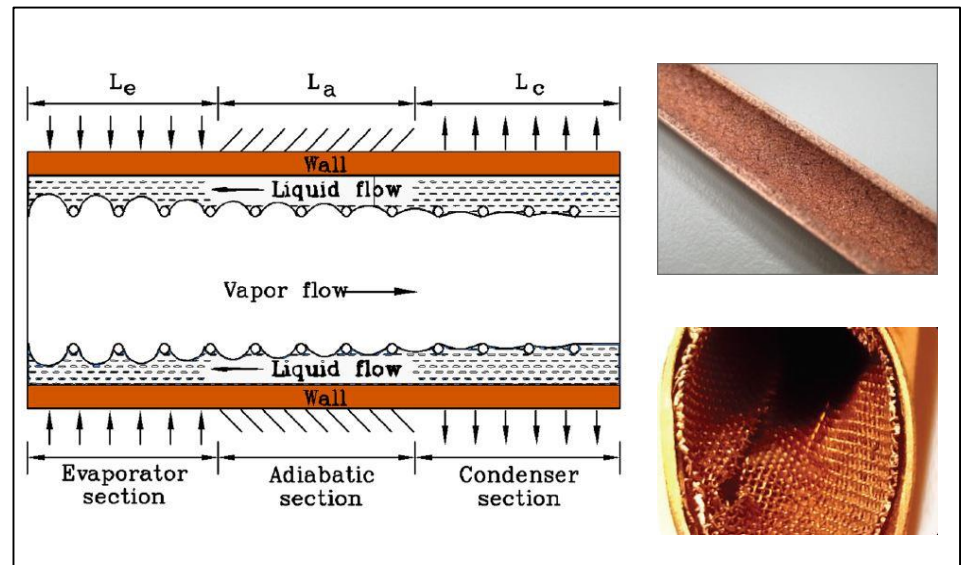
Competition between **Sorption** rate (surface tension) and vapour **transformation** rate (Evaporation) – **Two Velocity Scales**

Application – Heat pipe

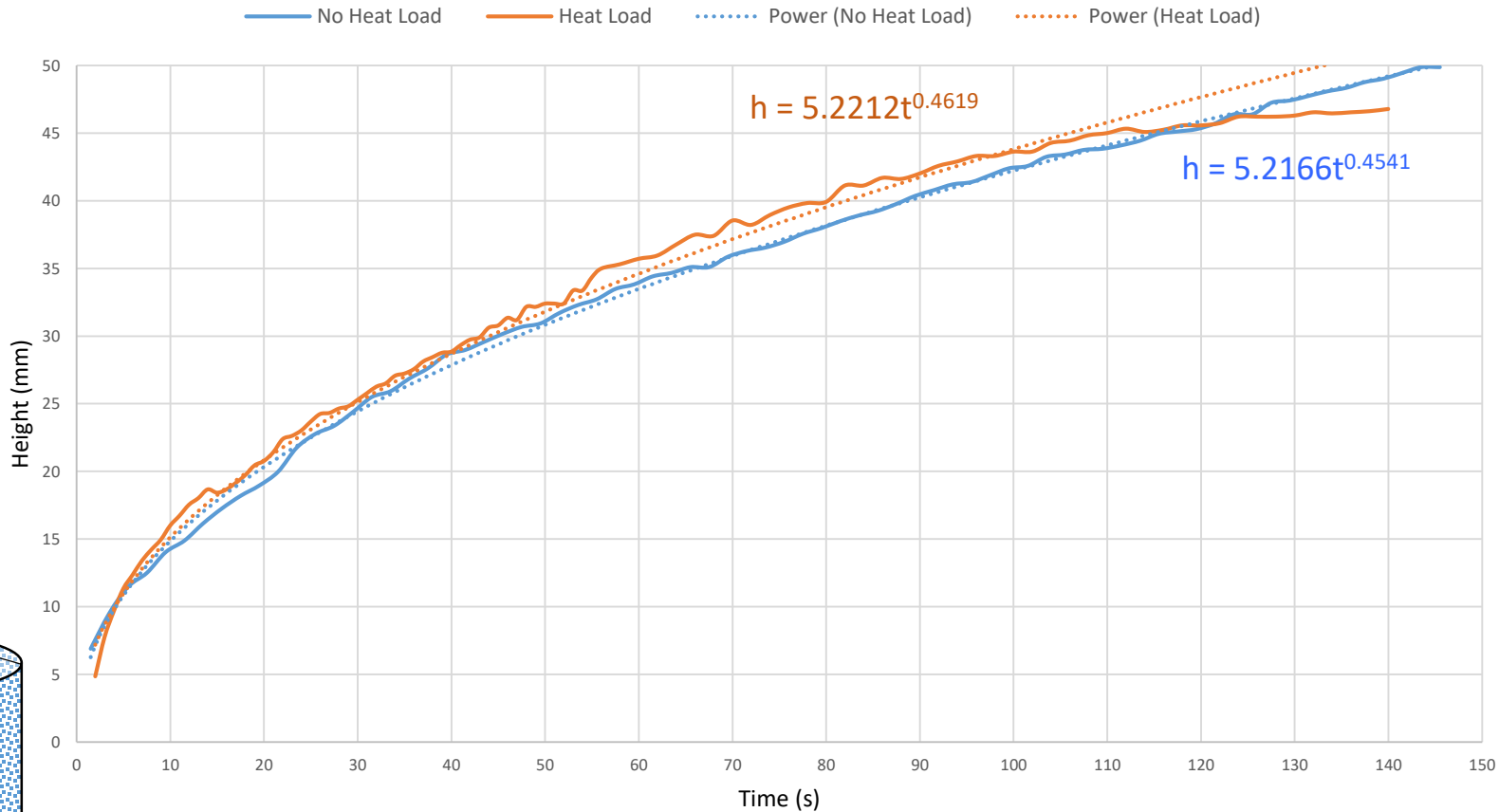
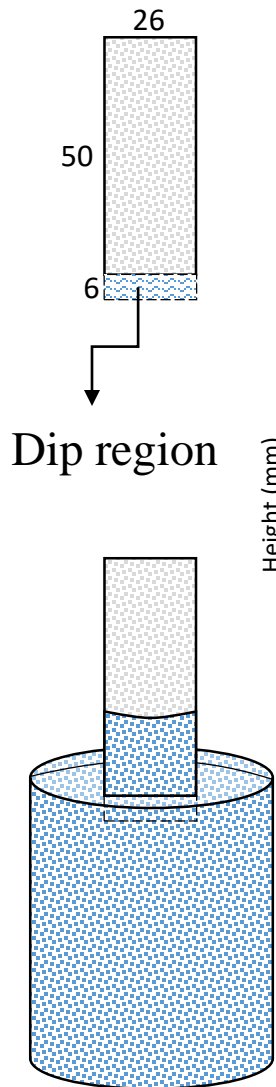
Kumar & Arakeri
(IJTS, 2020)



Faghri, 2005

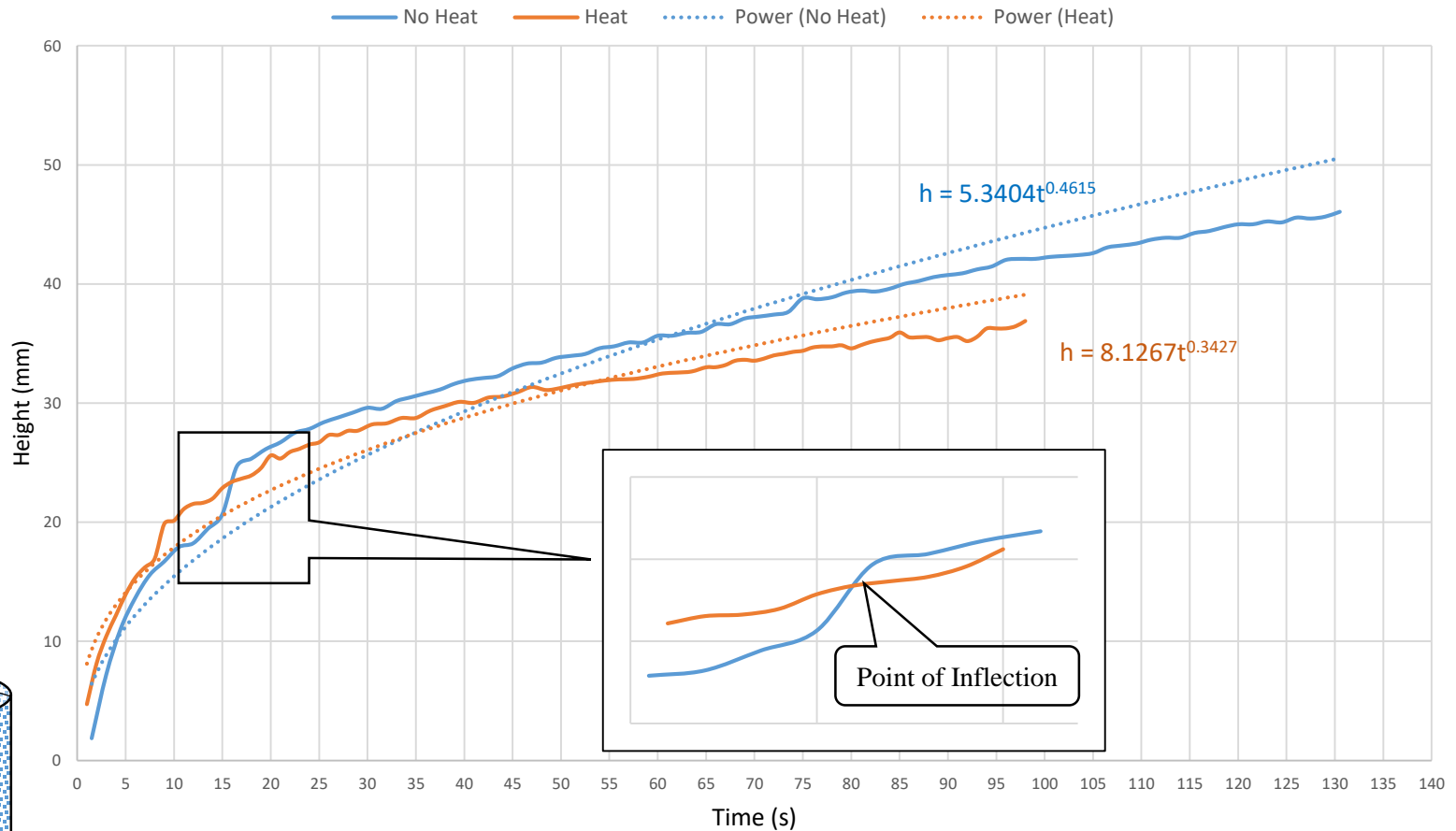
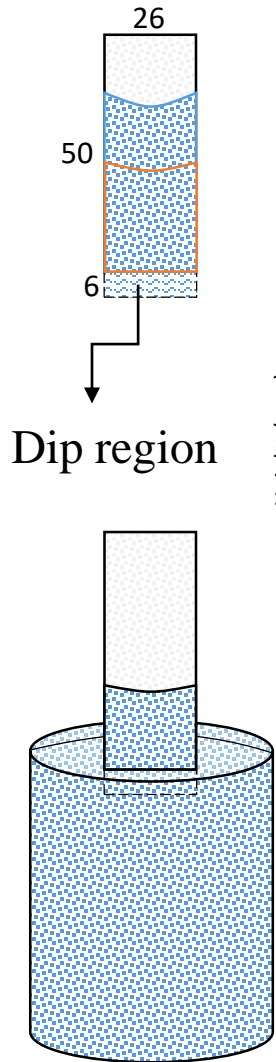


Results of Standard Liquid (Water)



No significant effect of heat load is seen on the rise of water in any experimental configurations – The **standard** liquid.

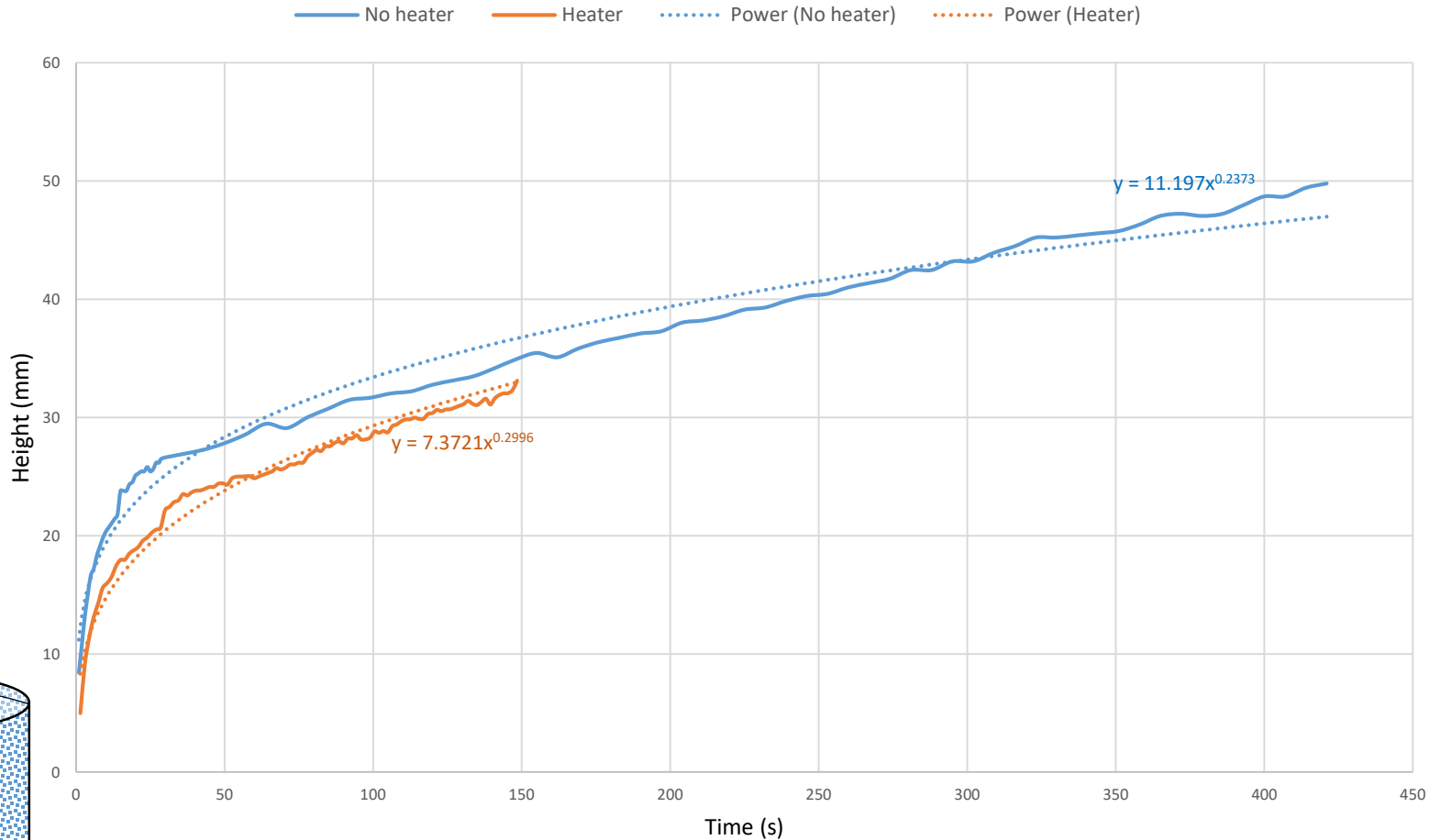
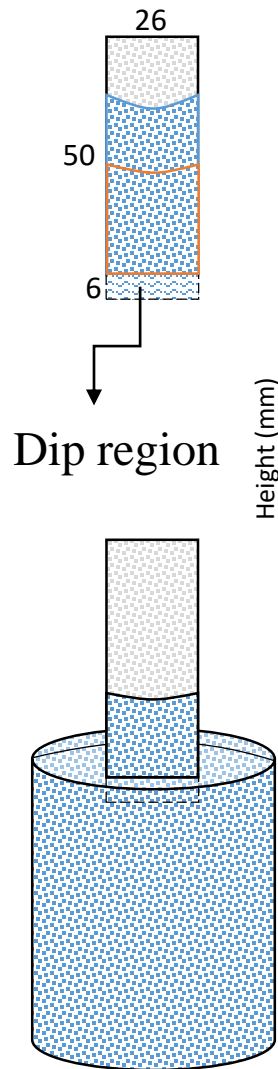
Results of Volatile Liquid (Pentane)



— Less velocity
Higher height rise

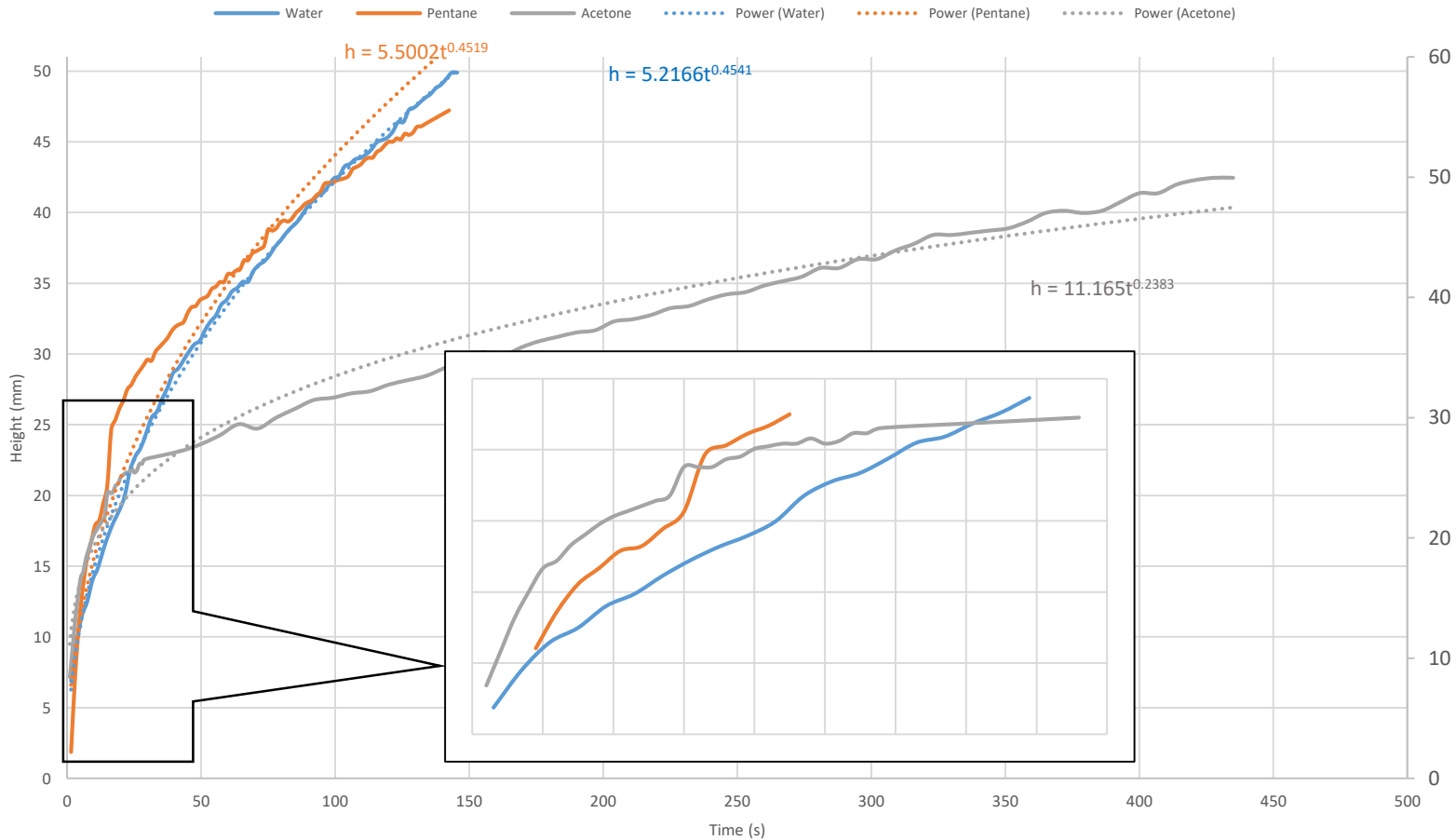
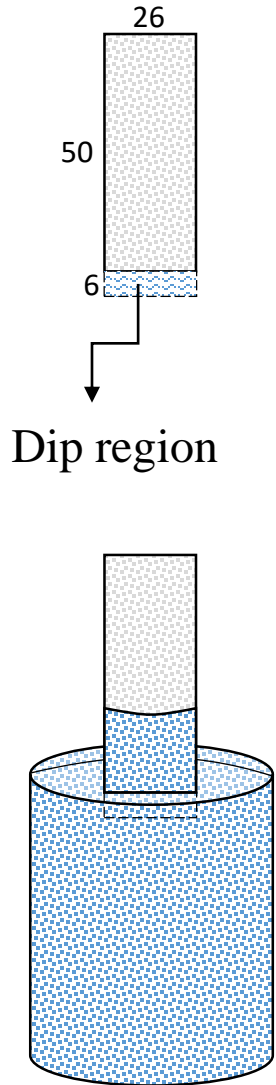
— High velocity
Lesser height rise

Results of Volatile Liquid (Acetone)

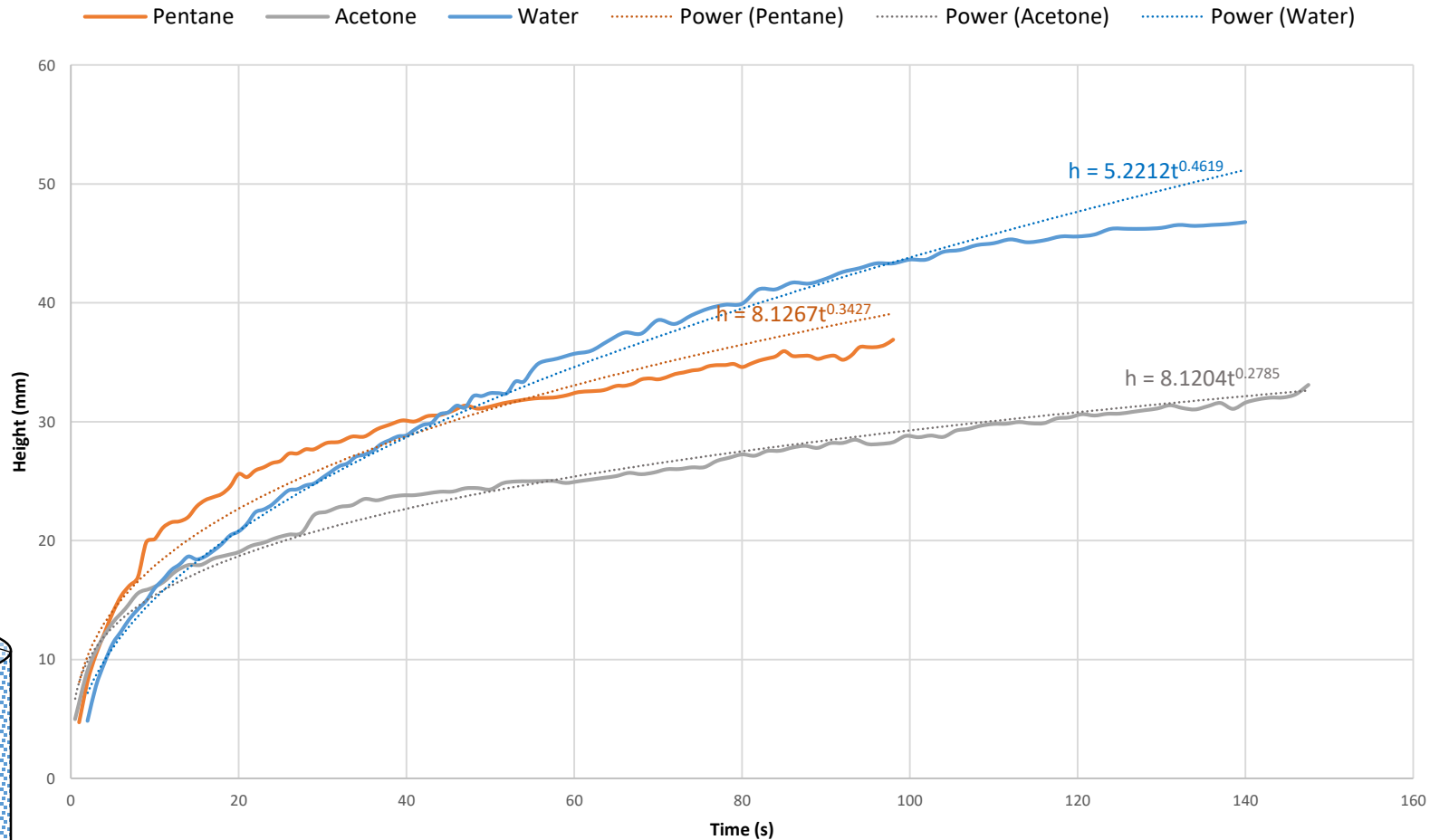
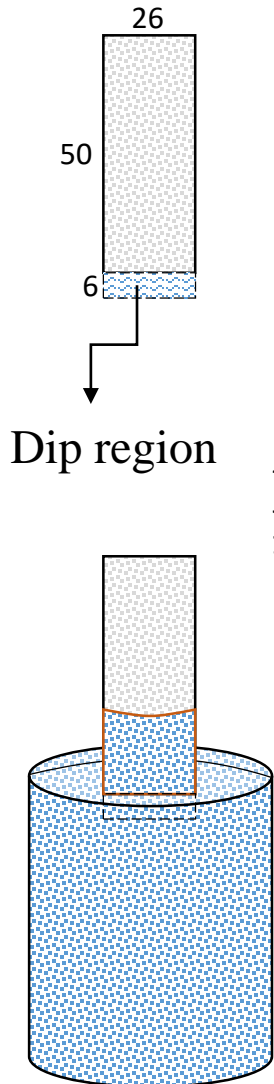


Hot acetone has **low velocity** and rises to **lower heights**

Comparison b/w Water, Pentane & Acetone (No Heat load)



Comparison b/w Water, Pentane & Acetone (Heat load)



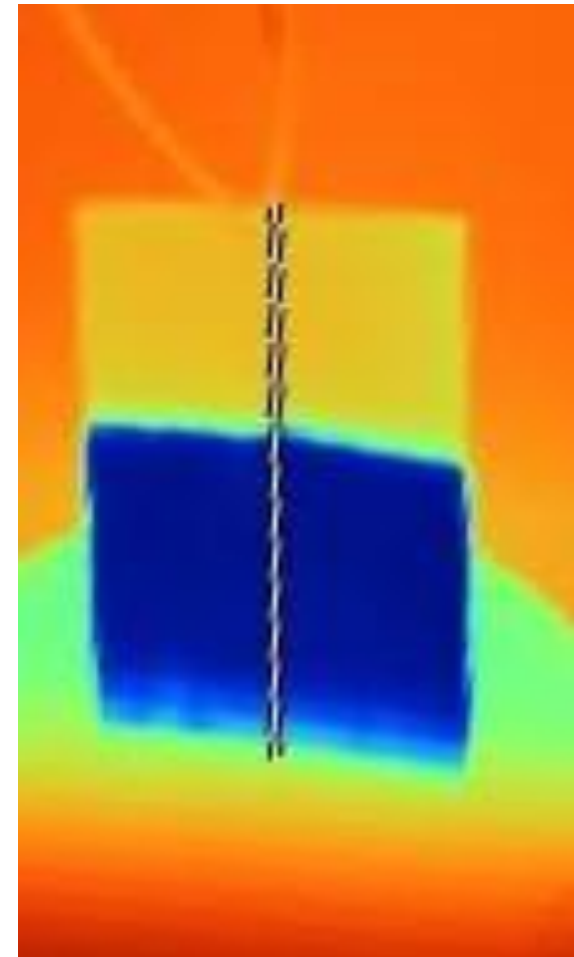
Liquid height rise – increase in the order – Acetone < Pentane < Water

Results of Volatile Liquid on sudden removal of heat load (Pentane)

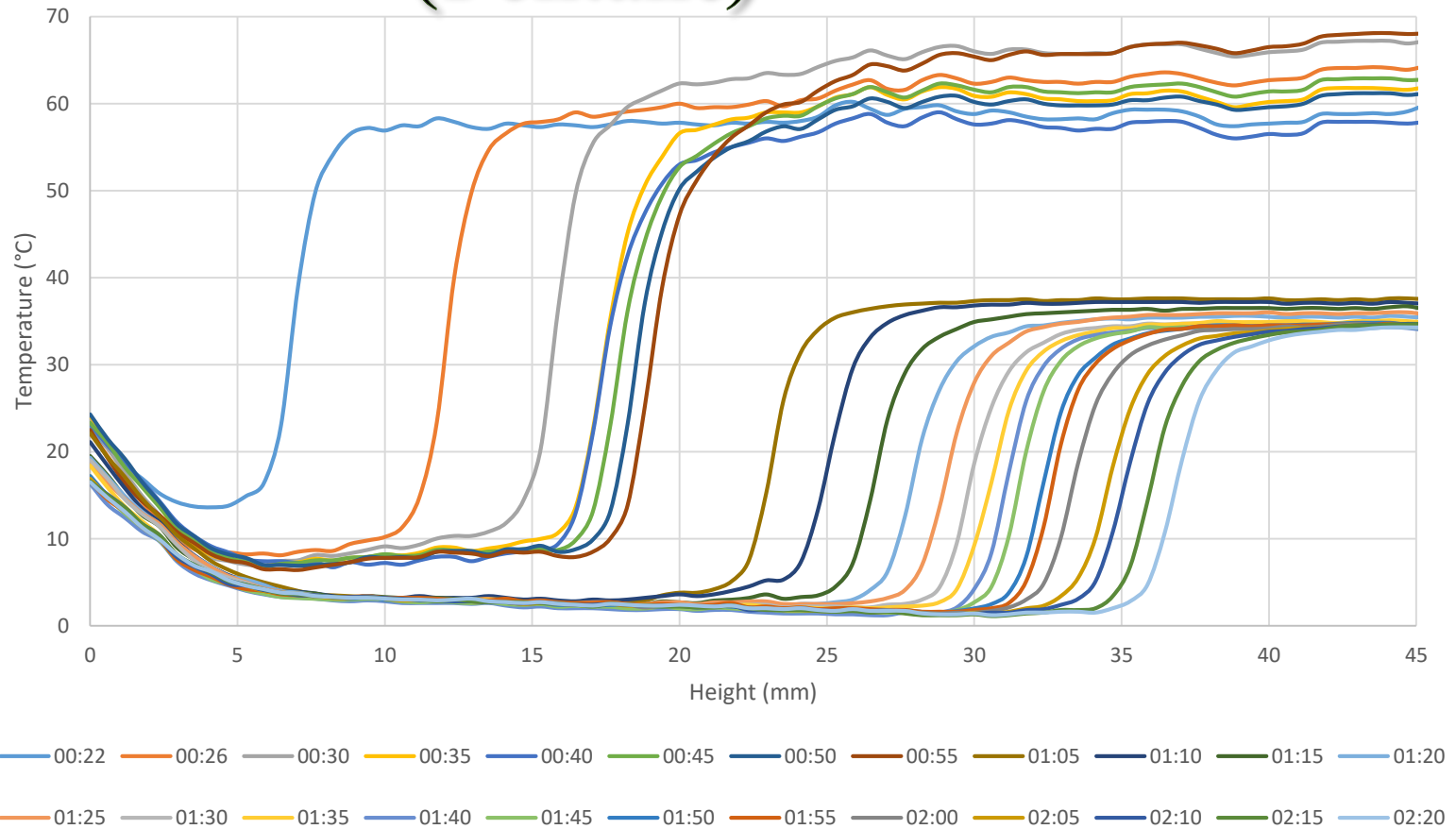
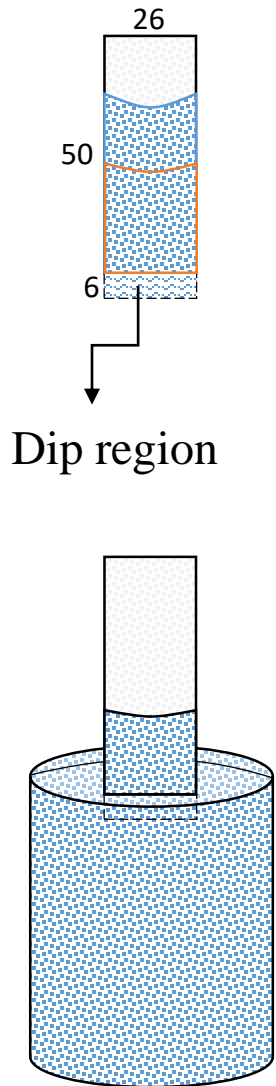
IR Video

IR Image

**Evaporation determines
the change in interface**

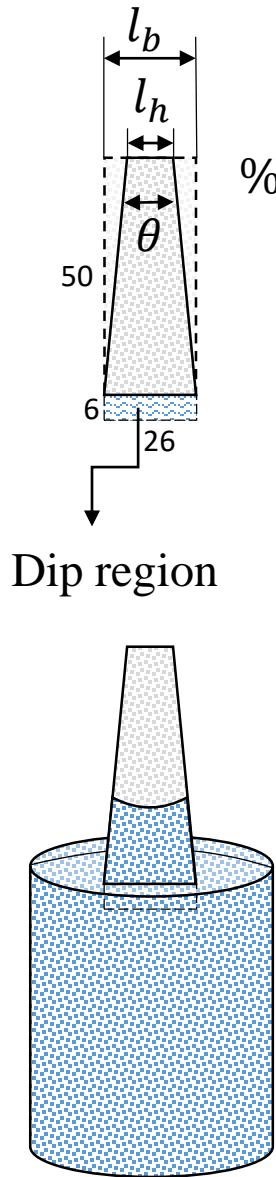


Results of Volatile Liquid on sudden removal of heat load (Pentane)

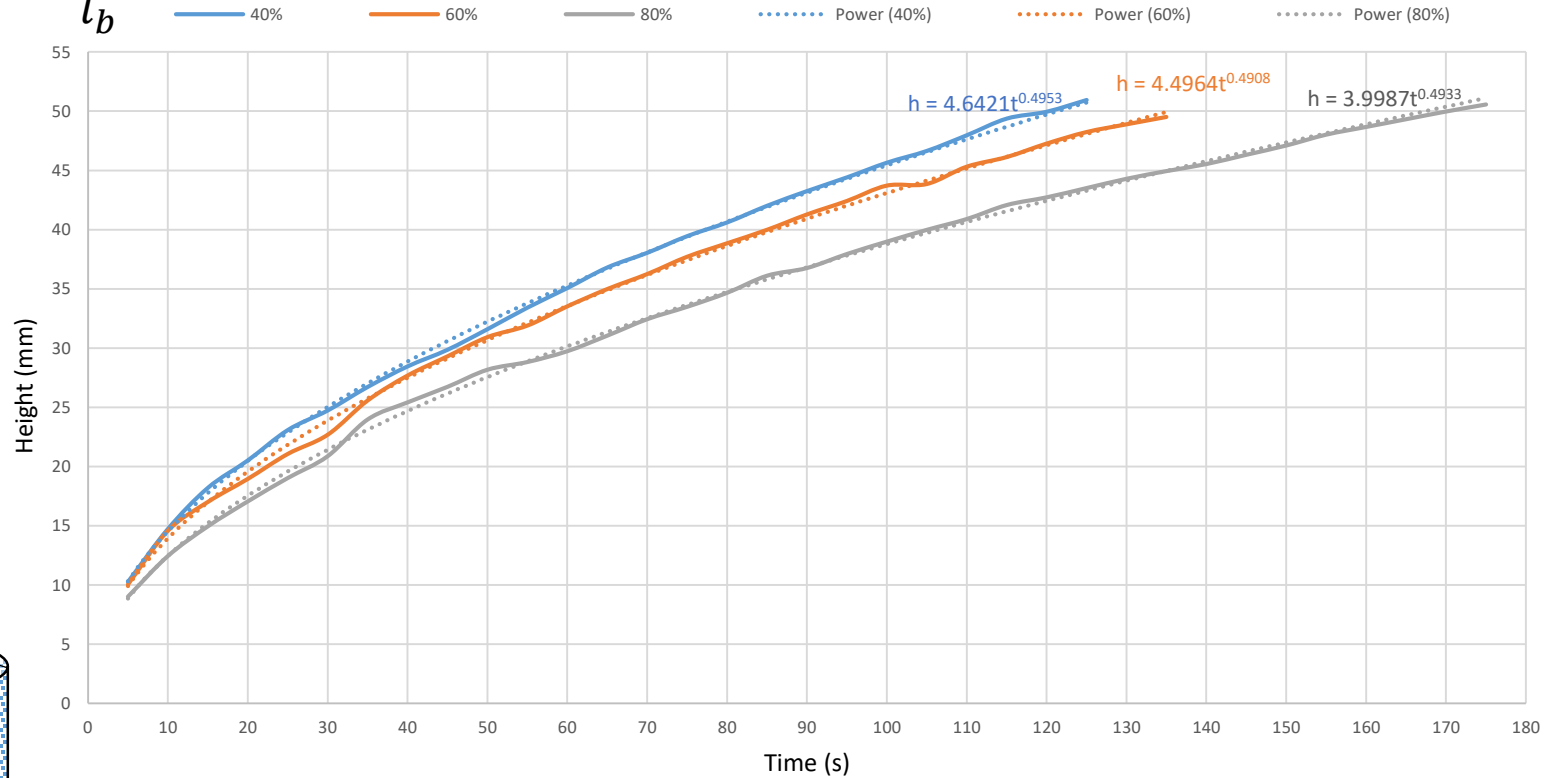


Increase in height – Removal of heat load

Results of Standard Liquid (Water) – Trapezium



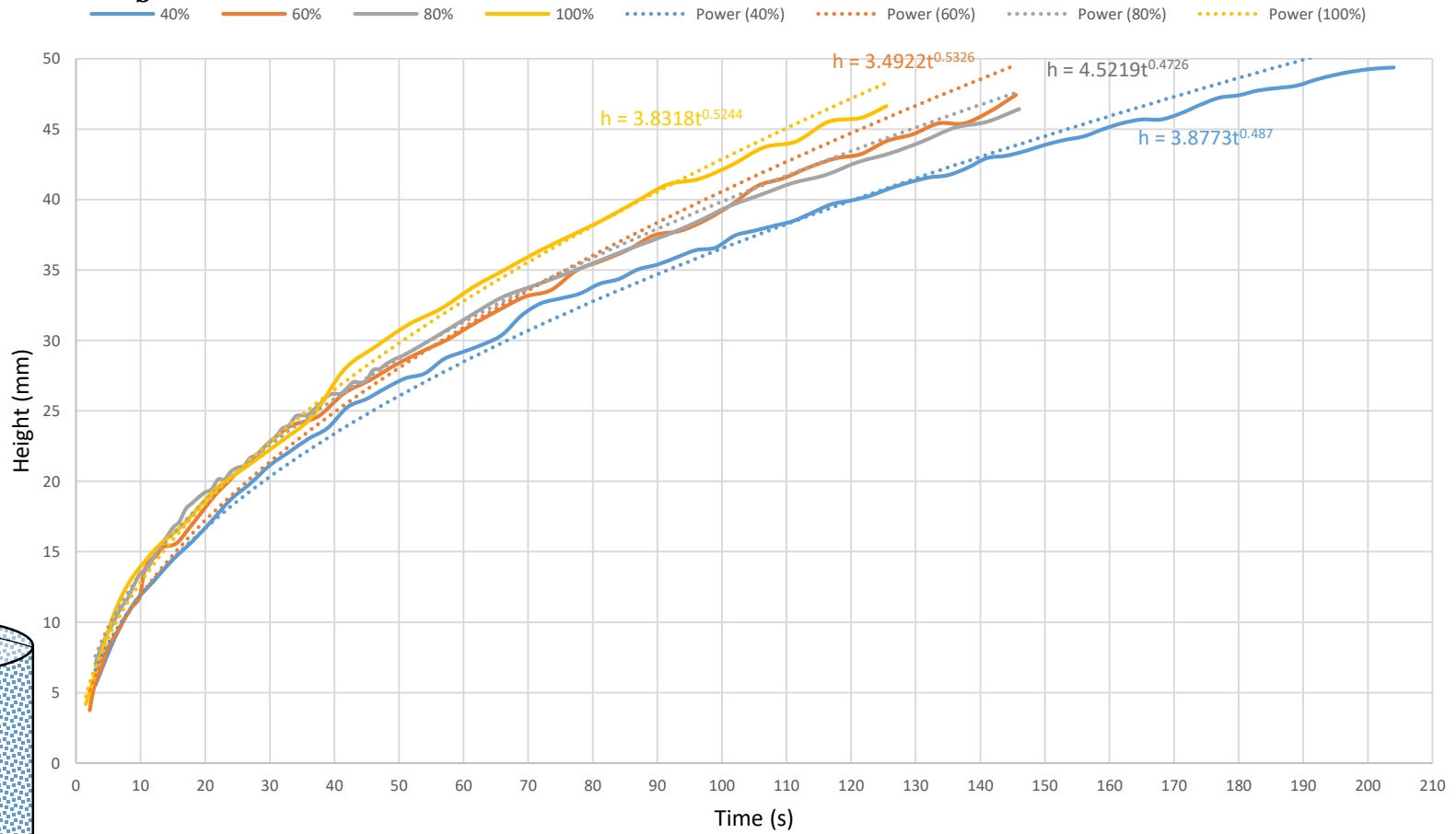
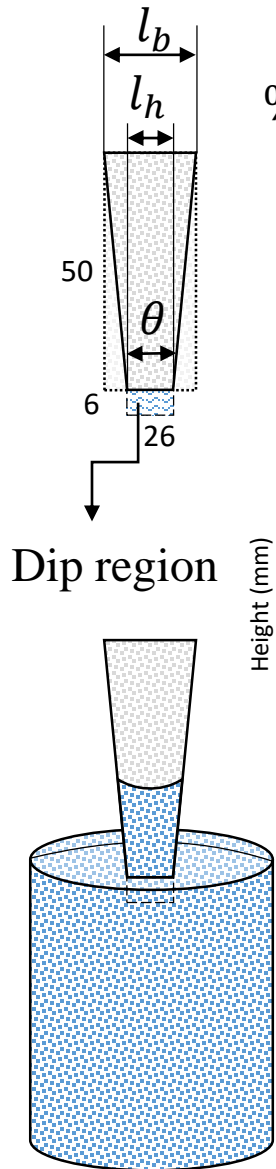
$$\% = \frac{l_h}{l_b} \times 100$$



$t \downarrow$ with $\theta \uparrow$

Results of Standard Liquid (Water) Inverted Trapezium

$$\% = \frac{l_h}{l_b} \times 100$$

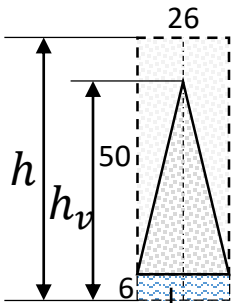


$t \downarrow$ with $\downarrow \theta$

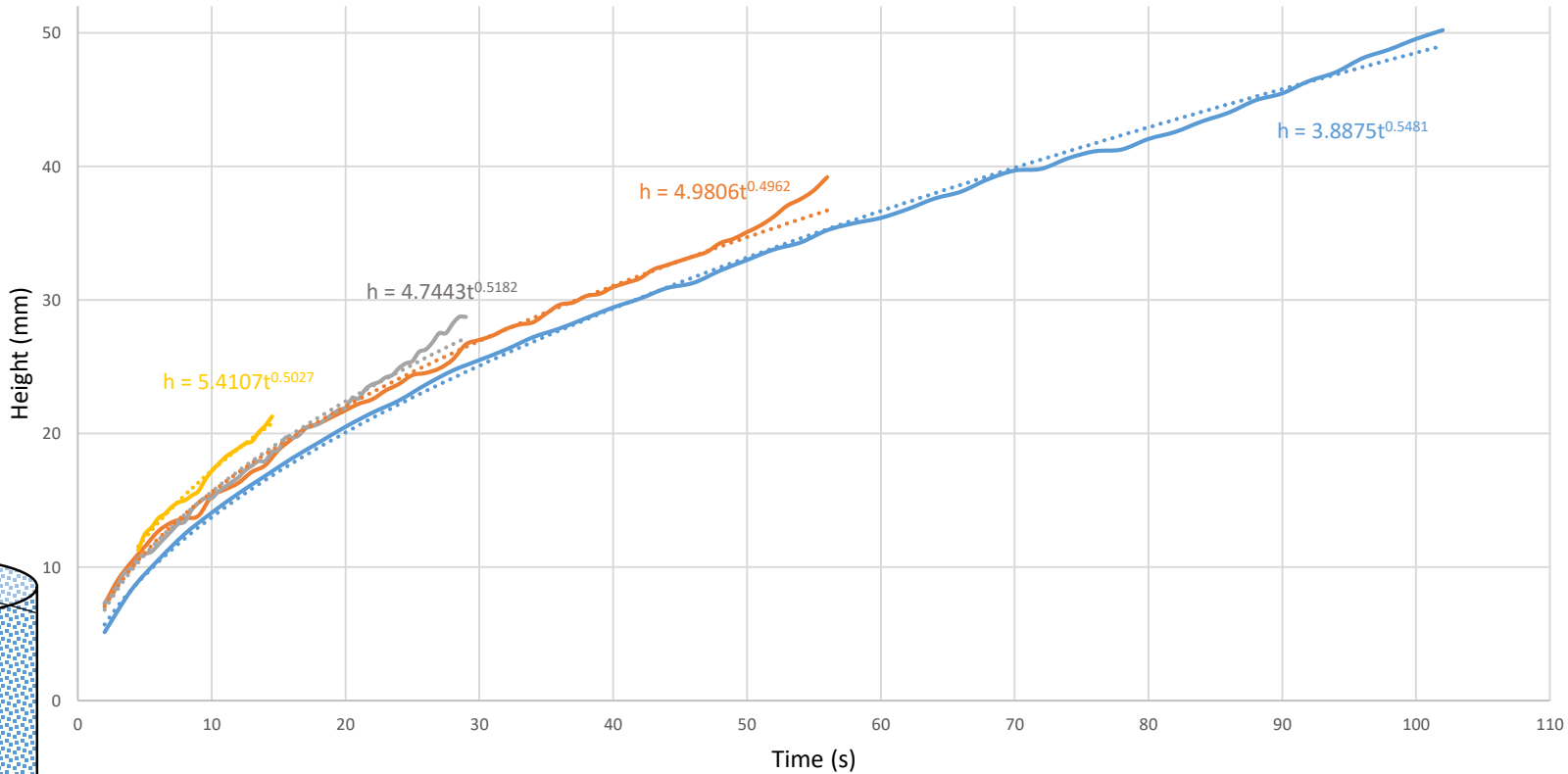
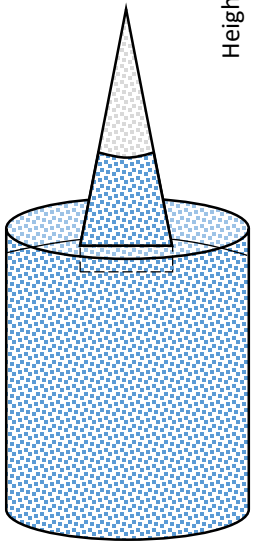
Results of Standard Liquid (Water) – Triangle

$$\% = -\frac{h_v}{h} \times 100$$

— 0%
 — -80%
 — -60%
 — -40%
 ⋯ Power (0%)
 ⋯ Power (-80%)
 ⋯ Power (-60%)
 ⋯ Power (-40%)

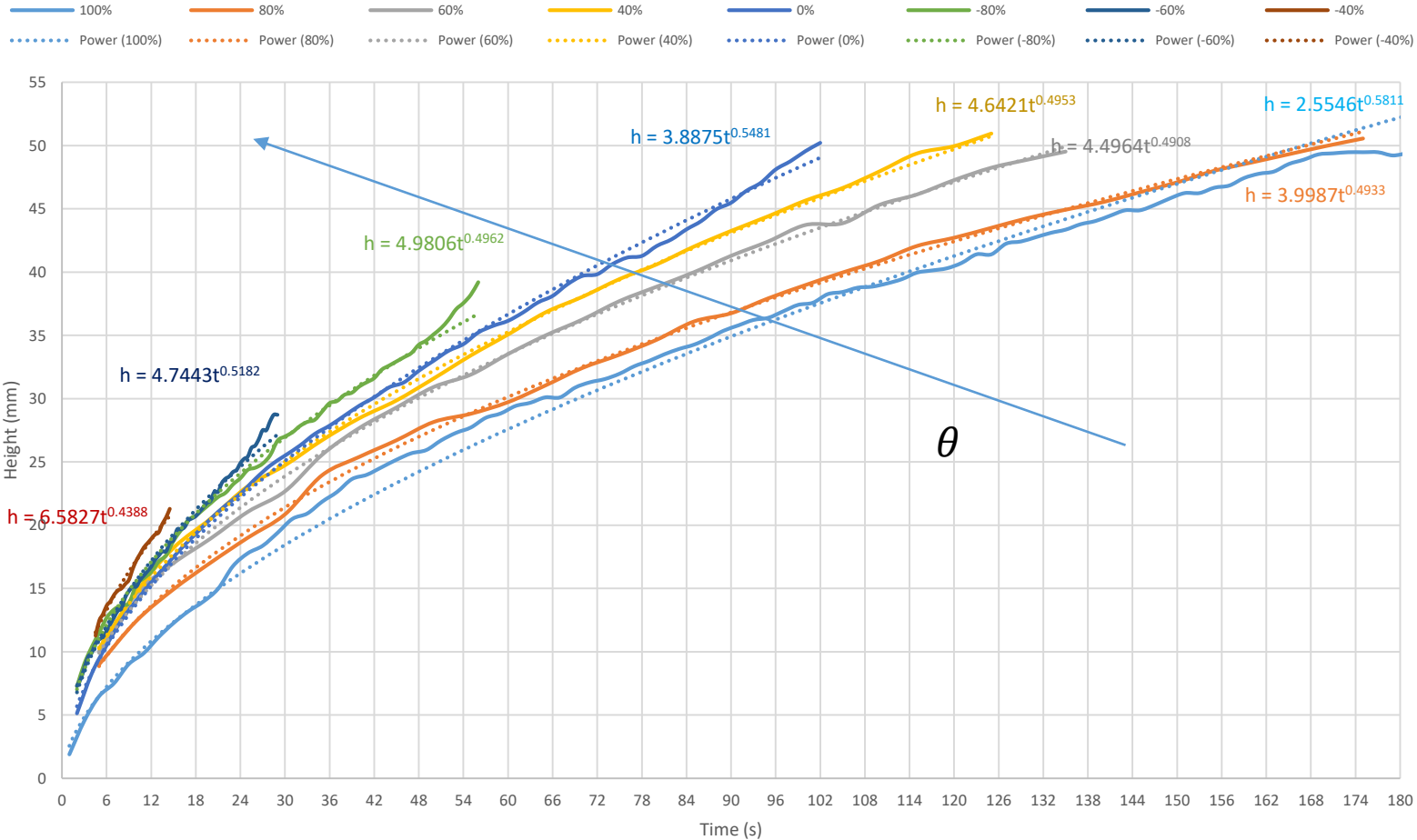
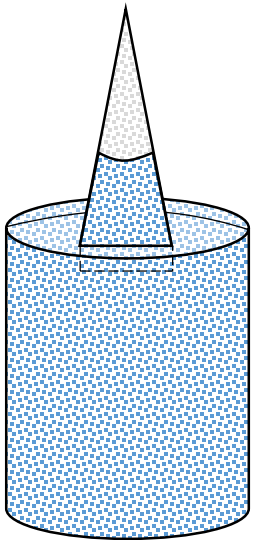
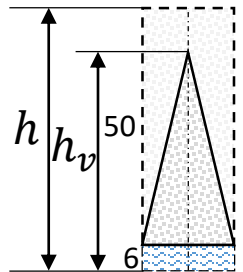
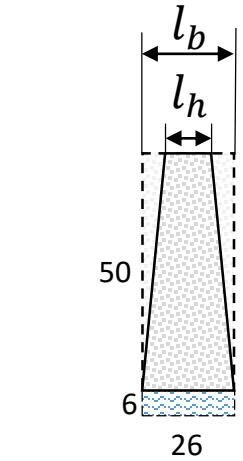


Dip region



$t \downarrow$ with $\uparrow \theta$ at tip of Δ ; $v \approx \alpha$

Comparison of Standard Liquid (Water) Trapezium & Triangle



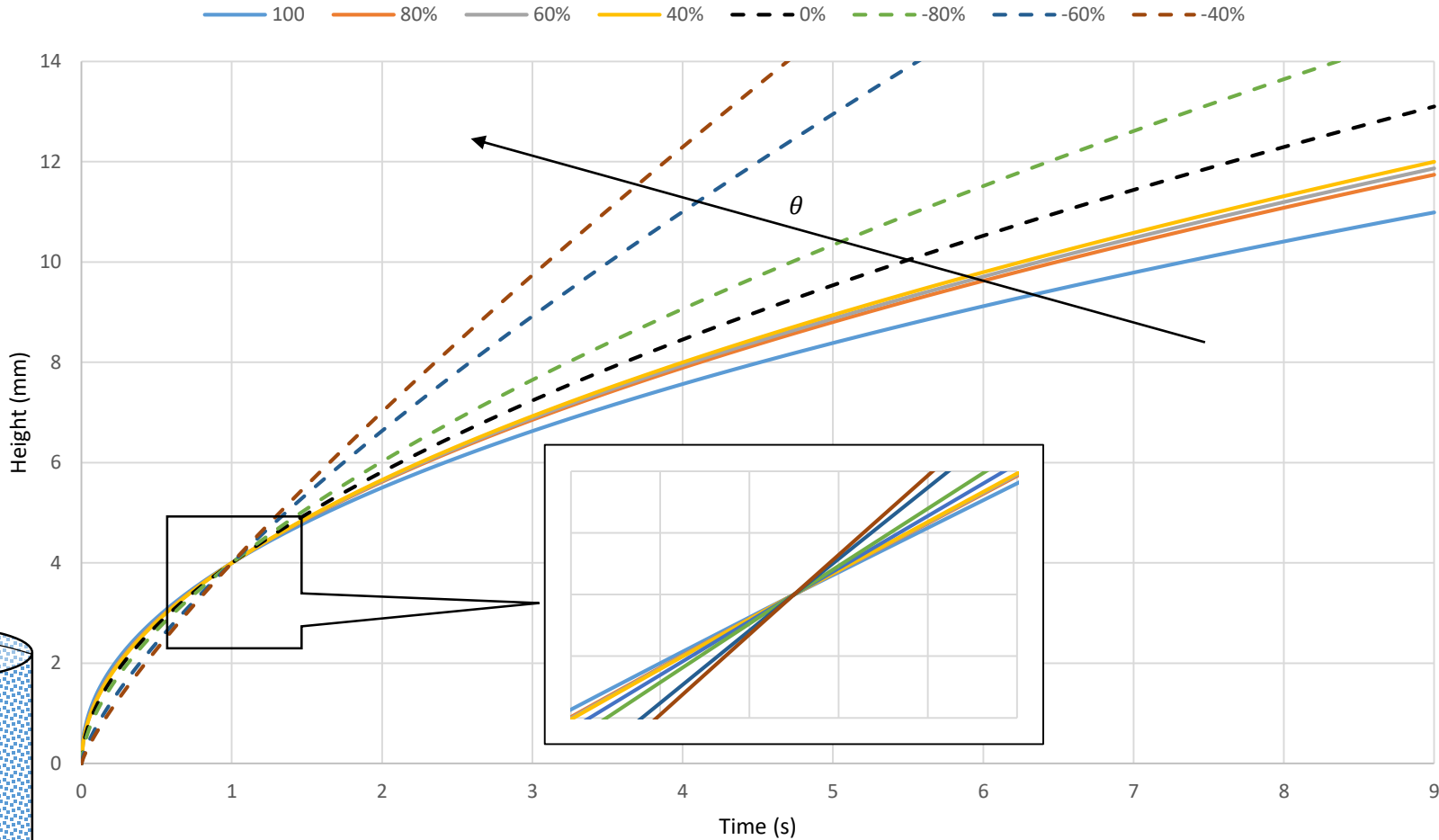
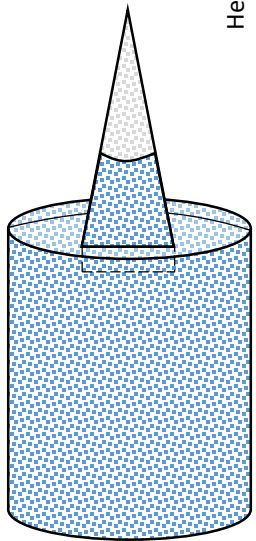
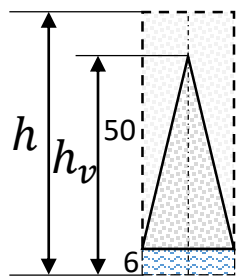
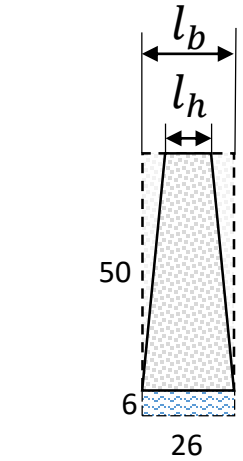
Short triangular geometries – BEST choice for liquid transportation

Comparison of Standard Liquid (Water) Trapezium & Triangle

Shape	%	Equation ($h = at^b$)	
		a	b
Rectangle	100	5.22	0.4541
Trapezium	80	4.59	0.4700
	60	4.25	0.5013
	40	3.67	0.5375
Triangle	100	3.82	0.5494
	80	3.47	0.5852
	60	2.12	0.7339
	40	1.72	0.8131

Triangular geometry **does not** follow $h \propto t^{0.5}$ law and in fact is closer to $h \propto t^1$
 $h \propto t^1$ can be easily achieved with **hyperbolically** converging geometries
 Careful choice of geometry – think **beyond** $h \propto t^{0.5}$ law !

Comparison of Standard Liquid (Water) Trapezium & Triangle (Ideal)



Increasing rate of liquid rise – Triangular > Trapezium > Rectangular

Conclusions

1. Liquid (Water, Pentane, and Acetone) rise **classical** experiments – a revisit.
2. Simple **2-D porous** networks to model **Heat pipes**, and its variants.
3. Various **geometries** – Rectangular, Trapezium, Triangles.
4. Initially, the liquid rise is same regardless of size and shape of filter paper.
5. Across all the experiments, $h \propto t^b$, $0.3 < b < 1$
6. For the same time, converging filter-papers showed higher h .
7. Converging geometries – **improve** the 'critical heat load' of wicks.
- 8. Rapid** liquid transportation – **Triangular** geometries are preferred.
9. For same time, diverging filter-papers showed lower h .
- 10. IR radiative** heating to boosts rate of evaporation.
11. Heating load **changes** the steady state interface position.
- 12. Evaporation** is indeed a **limiting factor** in wicks.
- 13. Huge implications in electronic cooling industries (Space crafts).**

Future Works

1. Different porosity and permeability systems.
2. Horizontal capillary spreading (non-linearly increasing area).
3. Heating method – conductive (**closer** to real heat pipes).
4. Mathematical model.

Important Contributions

1. Laplace (1806)
2. Lucas (1918)
3. Edward W Washburn (1921)
4. Levine (1980)
5. B. V. Zhmud (2000)
6. A Ponomarenko (2011)

Acknowledgements

1. Indian Institute of Science (IISc)
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