

The explicit filtering method for large eddy simulations of a turbulent premixed flame

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- Combustors operate in *lean premixed regime* to minimize pollutant emissions.
 - High Re flows, large range of energetic flow scales
 - Thin reaction zone (TRZ)
- Large Eddy Simulations of complex turbulent reacting flows
 - Capture dynamics of large flow structures and their interactions with flames
- Explicit filtering approach of LES (EFLES) is based on approximate deconvolution modelling (ADM).
 - Mathew et. al, *Phys. Fluids* 15 (8) (2003).
 - Applied successfully to non-reacting flow computations

- Governing Eq. for fully compressible, multi-component reacting flow in conservative form,

$$\frac{\partial \mathbf{U}}{\partial t} + \frac{\partial \mathbf{F}_i(\mathbf{U})}{\partial x_i} = \frac{\partial \mathbf{F}_{v,i}(\mathbf{U})}{\partial x_i} + \mathbf{S}(\mathbf{U}), \quad (1)$$

$$\mathbf{U} = [\rho \ \rho u \ \rho v \ \rho w \ \rho e \ \rho Y_1 \ \dots \ \rho Y_N]^T, \quad \mathbf{S} = [0 \ 0 \ 0 \ 0 \ 0 \ \dot{\omega}_1 \ \dots \ \dot{\omega}_N]^T.$$

- Eq. for LES field, $\bar{\mathbf{U}} = G * \mathbf{U}$,

$$\frac{\partial \bar{\mathbf{U}}}{\partial t} + \frac{\partial \mathbf{F}_i(\bar{\mathbf{U}})}{\partial x_i} = \frac{\partial \mathbf{F}_{v,i}(\bar{\mathbf{U}})}{\partial x_i} + \mathbf{S}(\bar{\mathbf{U}}) + \underbrace{\mathcal{R}(\mathbf{U}, \bar{\mathbf{U}}) + \mathcal{R}_S(\mathbf{U}, \bar{\mathbf{U}})}_{\text{remainder terms}}.$$

- G - low pass spatial filter.

- ADM uses $\mathbf{U} \approx \mathbf{U}^* = Q * \bar{\mathbf{U}}$ to get, $[Q \approx G^{-1}]$

$$\frac{\partial \bar{\mathbf{U}}}{\partial t} = G * \left\{ - \frac{\partial \mathbf{F}_i(\mathbf{U}^*)}{\partial x_i} + \frac{\partial \mathbf{F}_{v,i}(\mathbf{U}^*)}{\partial x_i} + \mathbf{S}(\mathbf{U}^*) \right\} = G * \mathcal{L}(\mathbf{U}^*),$$

- Stolz, Adams, *Phys. Fluids* 11 (7) (1999).

- Numerical solution of ADM Eq., with timestep Δt ;

- 1 Deconvolution: $\mathbf{U}^{*(n)} = Q * \bar{\mathbf{U}}^{(n)}$

- 2 Numerical Integration:

$$\begin{aligned} \bar{\mathbf{U}}^{(n+1)} &= \bar{\mathbf{U}}^{(n)} + \Delta t [G * \mathcal{L}(\mathbf{U}^{*(n)})] \\ \Rightarrow \bar{\mathbf{U}}^{(n+1)} &= G * [\mathbf{U}^{*(n)} + \Delta t \mathcal{L}(\mathbf{U}^{*(n)})] + \underbrace{[\bar{\mathbf{U}}^{(n)} - G * \mathbf{U}^{*(n)}]}_{\text{neglect } [\because G * \mathbf{U}^* \approx G * \mathbf{U}]} \end{aligned}$$

3 stage ADM procedure

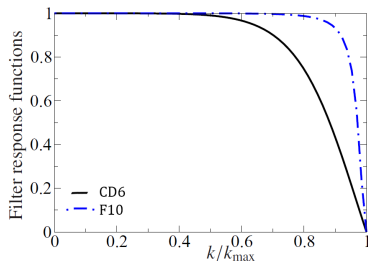
1. Deconvolution: $\mathbf{U}^{*(n)} = Q * \bar{\mathbf{U}}^{(n)}$
 2. Numerical Integration: $\mathbf{U}^{*(n)} \rightarrow \mathbf{U}^{*(n+1)}$
 3. Filtering: $\bar{\mathbf{U}}^{(n+1)} = G * \mathbf{U}^{*(n+1)}$
- Combine to an explicit filtering step
 $E = Q * G$
1. Deconvolution: $\mathbf{U}^{*(n+1)} = Q * \bar{\mathbf{U}}^{(n+1)}$

Explicit Filtering LES

- ① Numerical Integration: $\mathbf{U}^{*(n)} \rightarrow \mathbf{U}^{*(n+1)}$,
(using Eq. (1) in terms of \mathbf{U}^*)
- ② Filtering: Update $\mathbf{U}^{*(n+1)}$ with filtered field $E * \mathbf{U}^{*(n+1)}$
 - Mathew et. al, *Phys. Fluids* 15 (8) (2003).

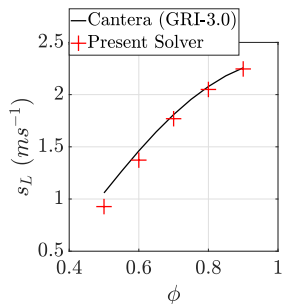
Explicit Filter

- $E \approx I$ over a range of large computed scales.
- E falls off to zero over a small range of the highest represented wavenumbers.
- As the represented spectral range is increased, EFLES ensures monotonic convergence to DNS.



Response Functions
Mathew, arXiv (2016)

- Discretization
 - 8th order central difference spatial discretization
 - 3rd order R-K time marching
- Explicit Filtering
 - 10th order spatial filter
- 13 species reduced chemical mechanism
 - Sankaran et. al, *Proc. Combust. Inst.* 31 (1) (2007)
- Navier-Stokes Characteristic Boundary Conditions (NSCBC)
 - Poinso, Lele, *J. Comp. Phys.* 101 (1) (1992)



Variation of s_L with ϕ for CH_4 -air premixed flames ($T_u = 800$ K, $p_0 = 1$ atm).

Filter Adaptation

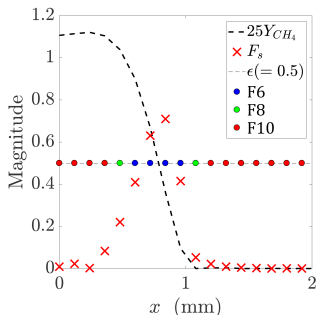
- Steep species gradients are detected using the sensor,

$$F_s = \left[\frac{\delta_F}{|Y_{CH_4,u} - Y_{CH_4,b}|} |\nabla Y_{CH_4}| \right] H \left(5.0 - \frac{\delta_F}{\Delta_{local}} \right).$$

- Progressively reduce filter order to 6 where $F_s \geq 0.5$.
- Adaption is performed along a mesh direction i when

$$\frac{\hat{x}_i \cdot \nabla Y_{CH_4}}{|\nabla Y_{CH_4}|} > \frac{1}{\sqrt{3}}.$$

- Patel, Mathew, *Fluids* 4 (3) (2019).



Computational Domain

Turbulent premixed CH₄-air round jet flame

- $\phi = 0.8$, $T_u = 800$ K

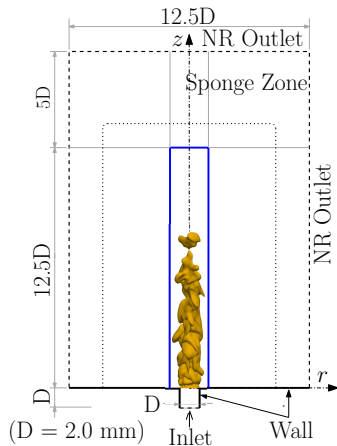
Laminar flame properties (from Cantera)

- $s_L = 2.05$ ms⁻¹, $T_b = 2313.65$ K

- $\delta_F = 300$ μ m, $\delta_H = 120$ μ m

Nominal mesh parameters

	Δ (μ m)	δ_F/Δ	δ_H/Δ	Points ($\times 10^6$)
DNS	30	10.0	4.0	29.2
LES4x	120	2.5	1.0	1.1
LES6x	180	1.7	0.7	0.5

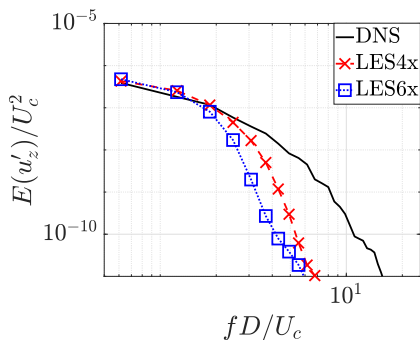


- Top hat mean axial velocity profile
 - $U_c = 65 \text{ ms}^{-1}$
 - $Re = U_c D / \nu = 1500$

- Inflow turbulence
 - Divergence free synthetic velocity fluctuations
 - ▶ Von Karman-Pao energy spectrum
 - Isotropic turbulence boxes are blended to generate a long dataset.
 - ▶ Larsson, *J. Comp. Phys.* 228 (2009)
 - Turbulent fluctuations are advected using *Taylor's hypothesis*

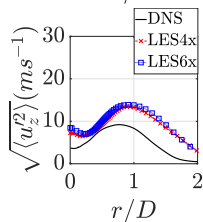
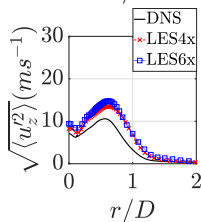
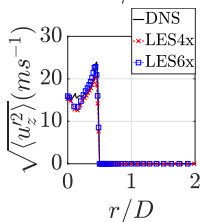
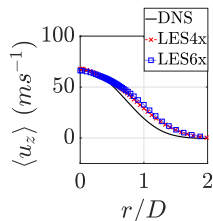
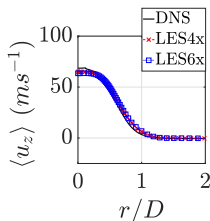
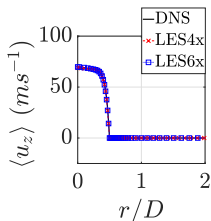
Results: Power Spectral Density

- PSD at low frequencies ($fD/U_c \leq 1$) are the same.
- Filter removes high wavenumber content in two LES cases.
- Monotonic convergence to DNS result is evident.
- Lack of wide inertial range due to low value of Re .



Normalised PSD on centerline at $z/D = 1.0$

Time averaged flow statistics



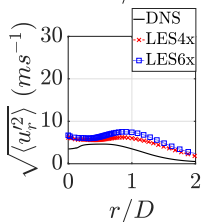
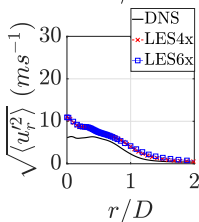
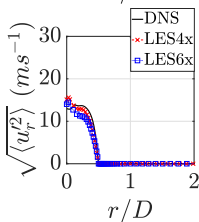
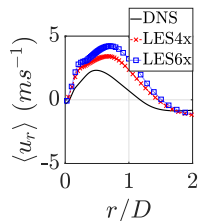
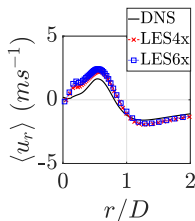
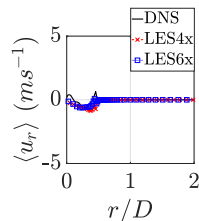
(a) $z/D = 0.0$

(b) $z/D = 2.0$

(c) $z/D = 5.0$

Time averaged statistics of streamwise velocity.

Time averaged flow statistics



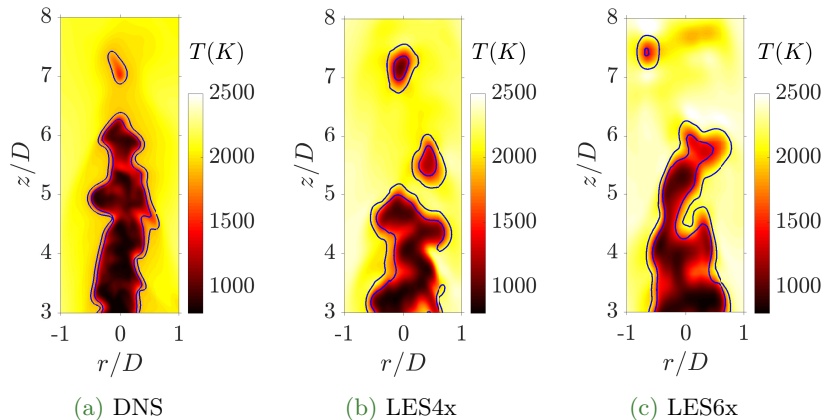
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(b) $z/D = 2.0$

(c) $z/D = 5.0$

Time averaged statistics of radial velocity.

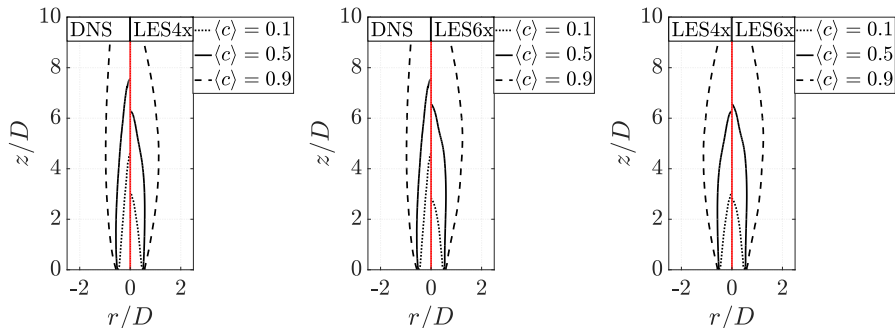
Instantaneous Snapshots



Typical instantaneous snapshots of temperature ($t \approx 4.0t_{FL}$) with the contour of Heat Release Rate, $\dot{q} = 5.0 \times 10^9 \text{ Js}^{-1}$.

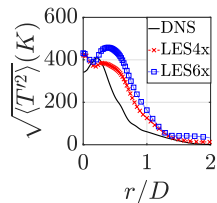
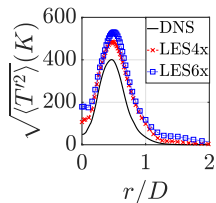
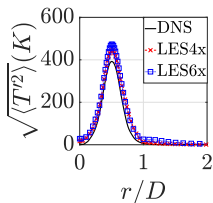
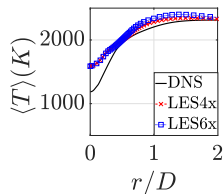
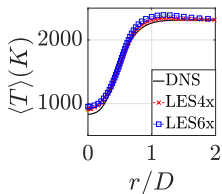
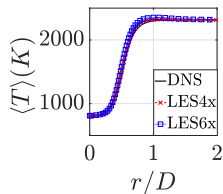
Mean Progress Variable Contours

- Small reduction in mean flame height in EFLES cases.
- LES results show thicker flame brush.



Contours of time averaged progress variable, $\langle c \rangle = \langle Y_{CO_2} \rangle / Y_{CO_2,b}$.

Time averaged statistics



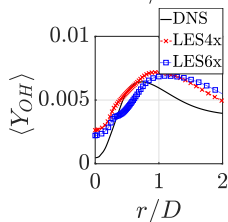
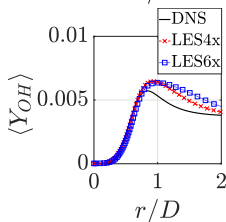
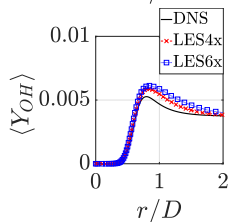
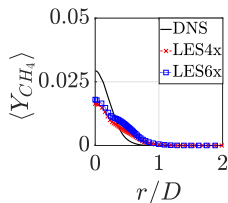
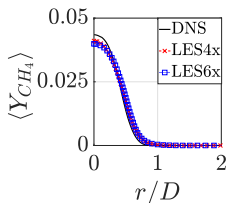
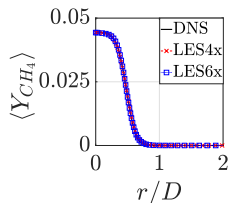
(a) $z/D = 1.0$

(b) $z/D = 2.0$

(c) $z/D = 5.0$

Time averaged statistics of temperature.

Time averaged statistics



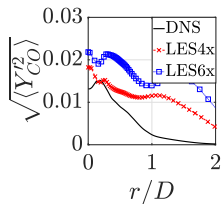
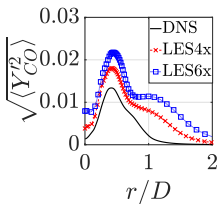
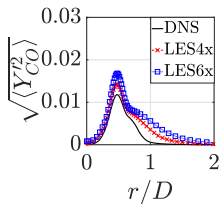
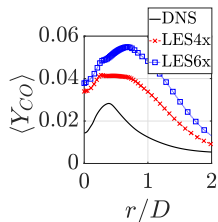
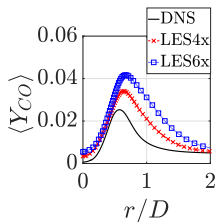
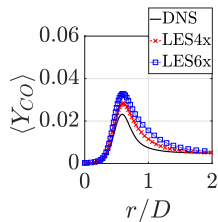
(a) $z/D = 1.0$

(b) $z/D = 2.0$

(c) $z/D = 5.0$

Time averaged statistics of CH_4 and OH mass fraction.

Time averaged statistics



(a) $z/D = 1.0$

(b) $z/D = 2.0$

(c) $z/D = 5.0$

Time averaged statistics of CO mass fraction.

- First application of EFLES approach to a simple realistic premixed jet flame configuration.
- LES results for velocity, temperature and major species show good qualitative and quantitative agreement.
- LES predicts a slightly shorter flame height and a moderately thicker flame brush.
- Use of QSS assumptions in present mechanism may lead to large deviations in CO prediction by EFLES computations.
- EFLES is a promising approach for LES of turbulent reacting flow as well.
- At high Re flows or when flame length scale is thinner than grid resolution, additional SGS model is needed for reaction rate terms (Ongoing work).